



***Modeling and Simulation
Transient Analysis Case Study
of a Liquids Gathering System***

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Description & Outline

- Numerous failures of a flexible composite pipeline
- Liquids gathering system
- Transient hydraulic model to evaluate a 4-inch flexible composite pipeline and an 8-inch steel pipeline

- ❖ Introduction

- ❖ Data Collection

- ❖ Computational Modeling

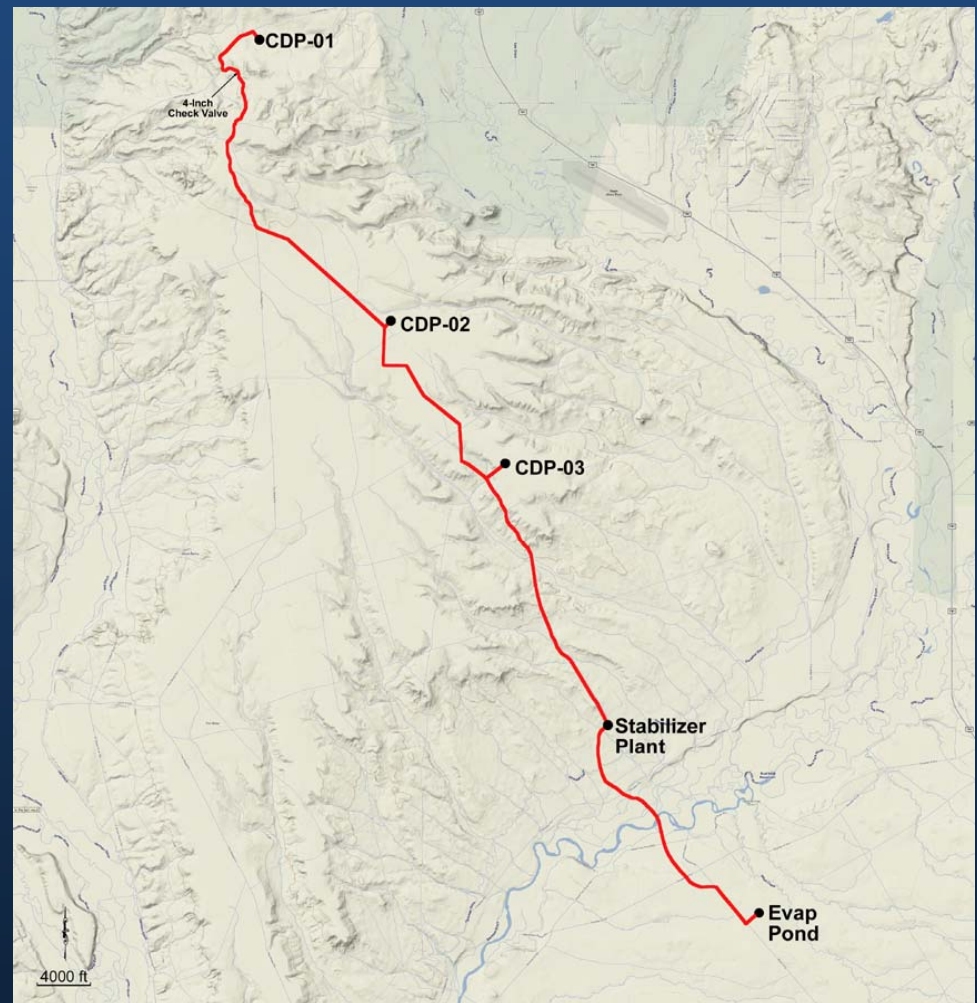
- ❖ Results

- ❖ Analysis

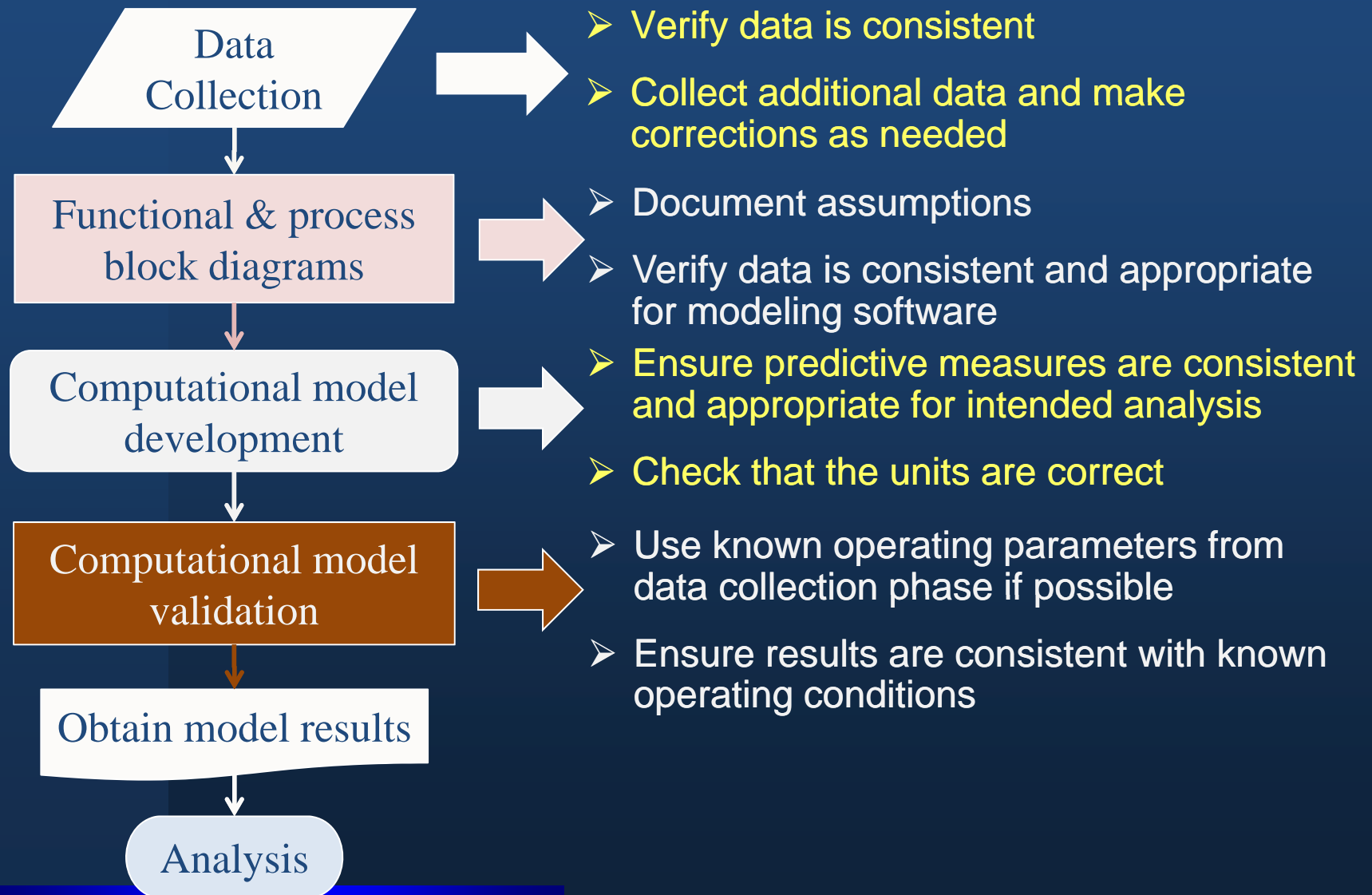
- ❖ Summary & Conclusions/Questions

Gathering System Map

- CDP-01, -02, -03, and Stabilizer plant
- CDPs identical in configuration with 2 triplex pumps (PDP)
- ~12.5 Miles from CDP-01 to stabilizer plant
- Stabilizer plant PCV holds 500 psig back pressure
- Check valve half way up hill
- ~500 ft from CDP-01 to top of hill



Modeling Process



Data Collection

The screenshot displays a software interface for data collection. At the top, a menu bar includes File, Edit, Setting, View, and Help. Below it is a toolbar with icons for New, Open, Save, Copy, Setup, Print, About, Start, Stop, Start WFL, Stop WFL, Start AVG, Stop AVG, Overlay, Peakhold, Live, Average, and Save. On the left, a tree view shows a project structure with folders for Imaginary, Process/Other, Channels, Tachs, and Locks. The main area contains two time plots. The top plot, titled 'Time Plot (Ch1)', shows pressure in PSI over 8 seconds with a peak-to-peak value of 39.68 V. The bottom plot, titled 'Time Plot (Ch2)', shows pressure in PSI over 8 seconds with a peak-to-peak value of 17.63 V. The status bar at the bottom indicates 'Ready' and 'PLAYBACK 1.00x' with a timestamp of 2008-09-23 16:41:31.

File Edit Setting View Help

New Open Save Copy Setup Print About Start Stop Start WFL Stop WFL Start AVG Stop AVG Overlay Peakhold Live Average Save

Imaginary
Process/Other
Mimic
Field
Alert
Mini-Bars
Alarm Logs
Results List
Table Tags
Script
Channel Information

Channels
1:
2:
3:
4:
5:
6:
7:
8:
9:
10:
11:
12:
13:
14:
15:
16:
Tachs
1: Tach 1
2: Tach 2
3: Tach 3
4: Tach 4
Locks
Lock 1
Lock 2
Lock 3

Project Graphs Settings

Time
Time Plot (Ch1)
PSI
520.0
505.0
490.0
475.0
460.0
0.000 8.000
2.1797 Sec, 488 PSI
PEAK-TO-PEAK: 39.68 V

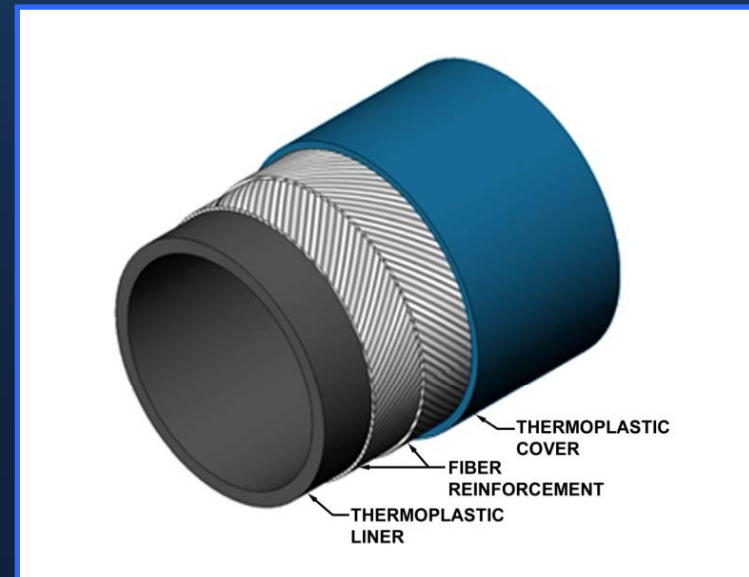
Time
Time Plot (Ch2)
PSI
500.0
492.5
485.0
477.5
470.0
0.000 8.000
PEAK-TO-PEAK: 17.63 V

Ready
PLAYBACK 1.00x 2008-09-23 16:41:31

Documentation

- ❖ P&IDs and isometric diagrams
- ❖ Datasheets
- ❖ Operational philosophy
- ❖ Reports
- ❖ Anecdotal data
 - Failures appeared to increase after check valve installed

Flexible Pipe Structural Components



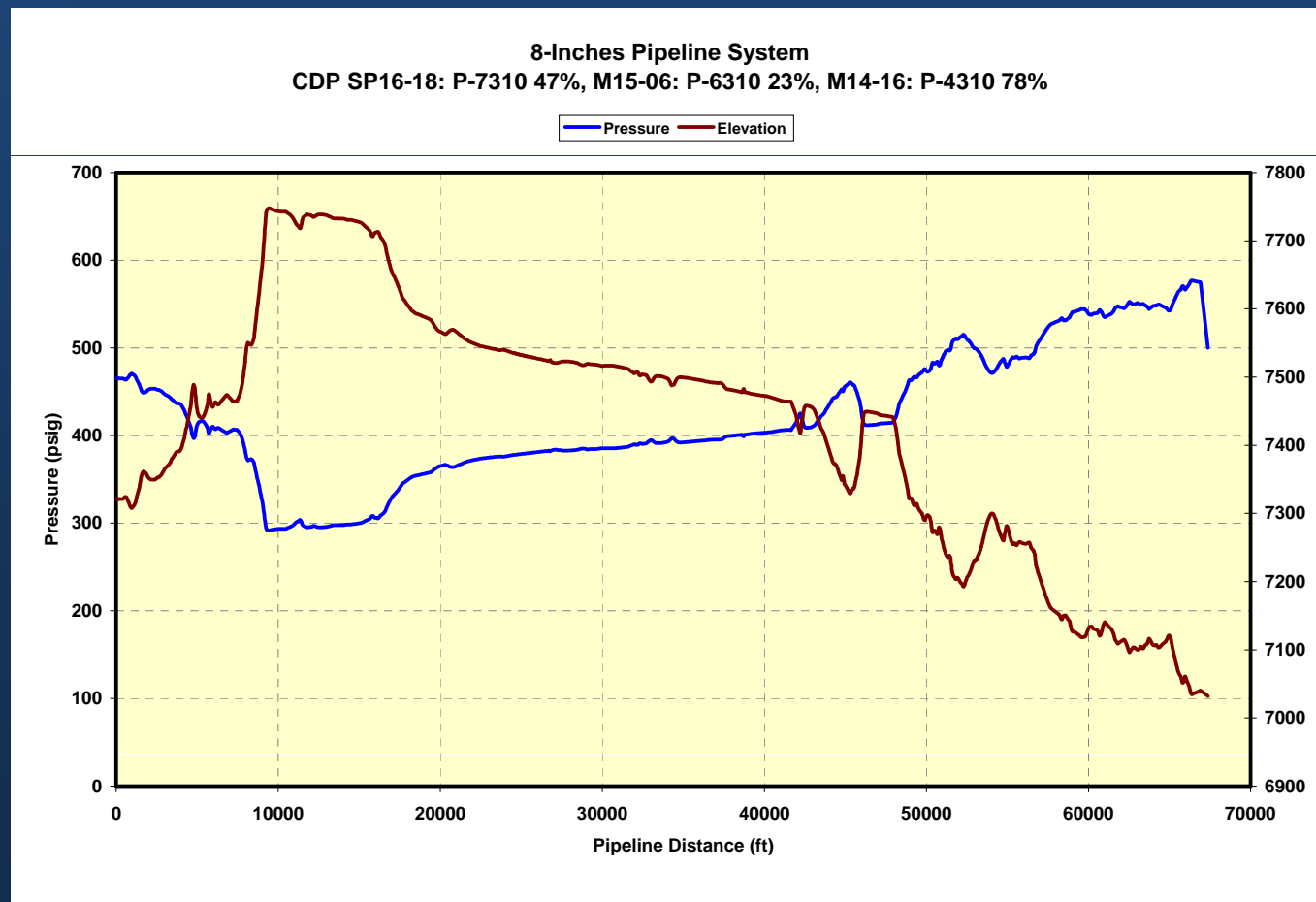
Field Survey

- ❖ Verified documentation and collected additional information
- ❖ Instrumented all three CDPs
- ❖ Did not go to stabilizer plant

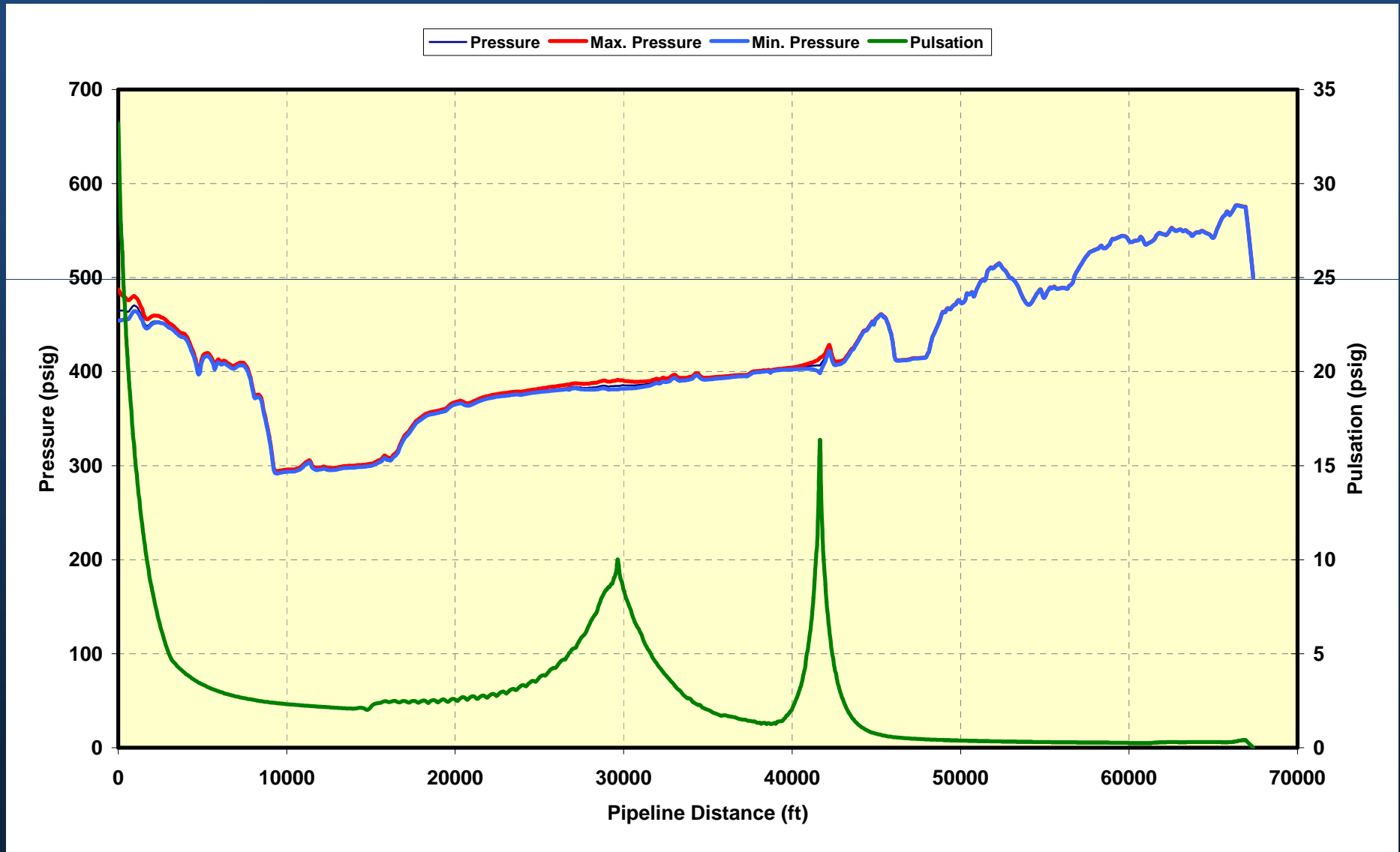


Transient Hydraulic Modeling

- ❖ Utilized the Stoner Pipeline Simulator (SPS)
- ❖ Slightly compressible liquids EOS



8-Inch Pipeline System Pressure with Pulsation



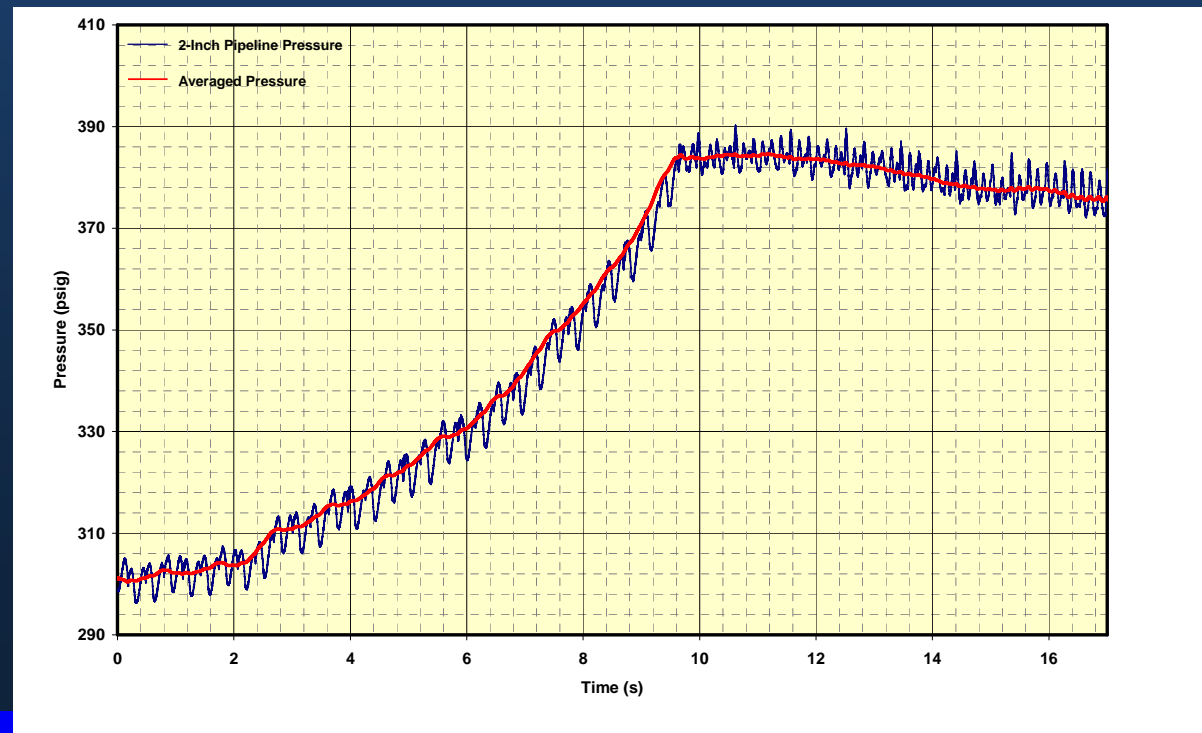
Summary Results

- ❖ The results did not reveal a problem related to water-hammer in either the pre-existing or existing pipelines
- ❖ The pulsations were a little high in the pre-existing pipeline, but were not considered excessive
- ❖ Transients during pump start and stops were significant but were well within the limits of the pipeline
- ❖ An investigation of failed composite pipeline sections revealed the failure occurred from the inside outward
- ❖ There was no creep, and adjacent sections were burst tested to greater than 2 times the MAOP

Water Hammer Analysis

- ❖ Water hammer not a problem
 - Flow velocities are low and therefore the momentum change is low
 - No mechanism found for causing any significant water hammer issues

2-in pipe Ramp-up
from 20%-100%

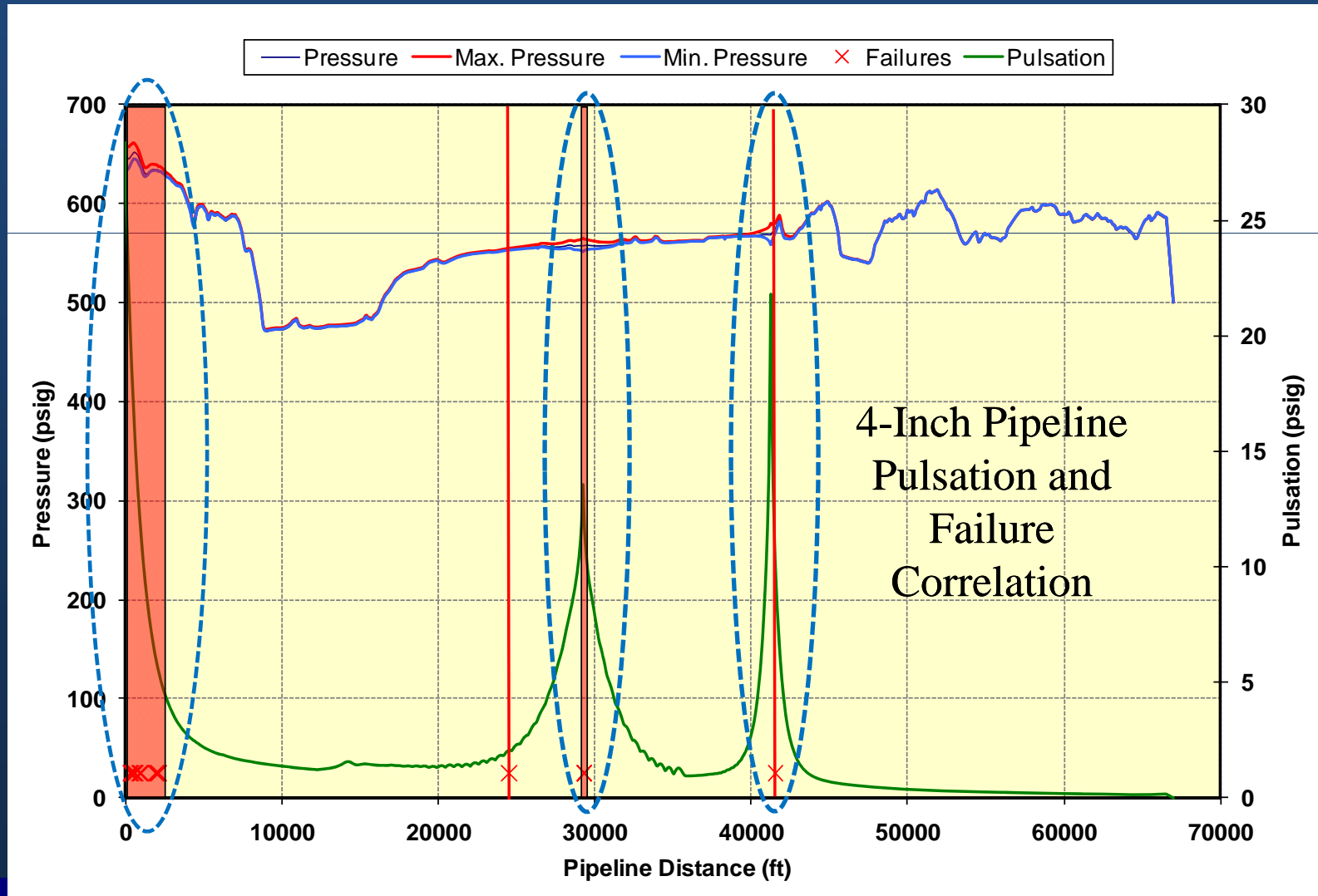


Transient Response Analysis

- ❖ Startup & shutdown transients not a problem
 - Several test cases were run which resulted in significant transient responses but were not enough to lead to a pipeline failure
 - There was no significant response related to the addition of the check valve half way up the hill
- ❖ Pulsation while small may play a significant part in the flexible composite pipeline failure

Pulsation Analysis

- ❖ Pulsations are strongly correlated failure sites



Failure Analysis

- ❖ Analysis of failed segments revealed failure from inside outward
- ❖ Inner-liner erupted through outer liner with little evidence of water between layers
- ❖ Hydro-testing of adjacent segments met or exceeded specifications
- ❖ Glass fibers near the inner liner tended to have jagged breaks whereas fibers near the outside tended to be clean breaks



Failure Assessment

- ❖ There appears to be no obvious failure mechanism
- ❖ Failures occur somewhat randomly and as soon as a failure is fixed another one appears
- ❖ However, the failures appear to correlate very well to the areas with the highest pulsation
- ❖ The pipe vendor warns that the pipe is not designed for use in cyclic application above 20% of rated pressure (Cyclic is defined as approximately once per day)

Failure Assessment, continued

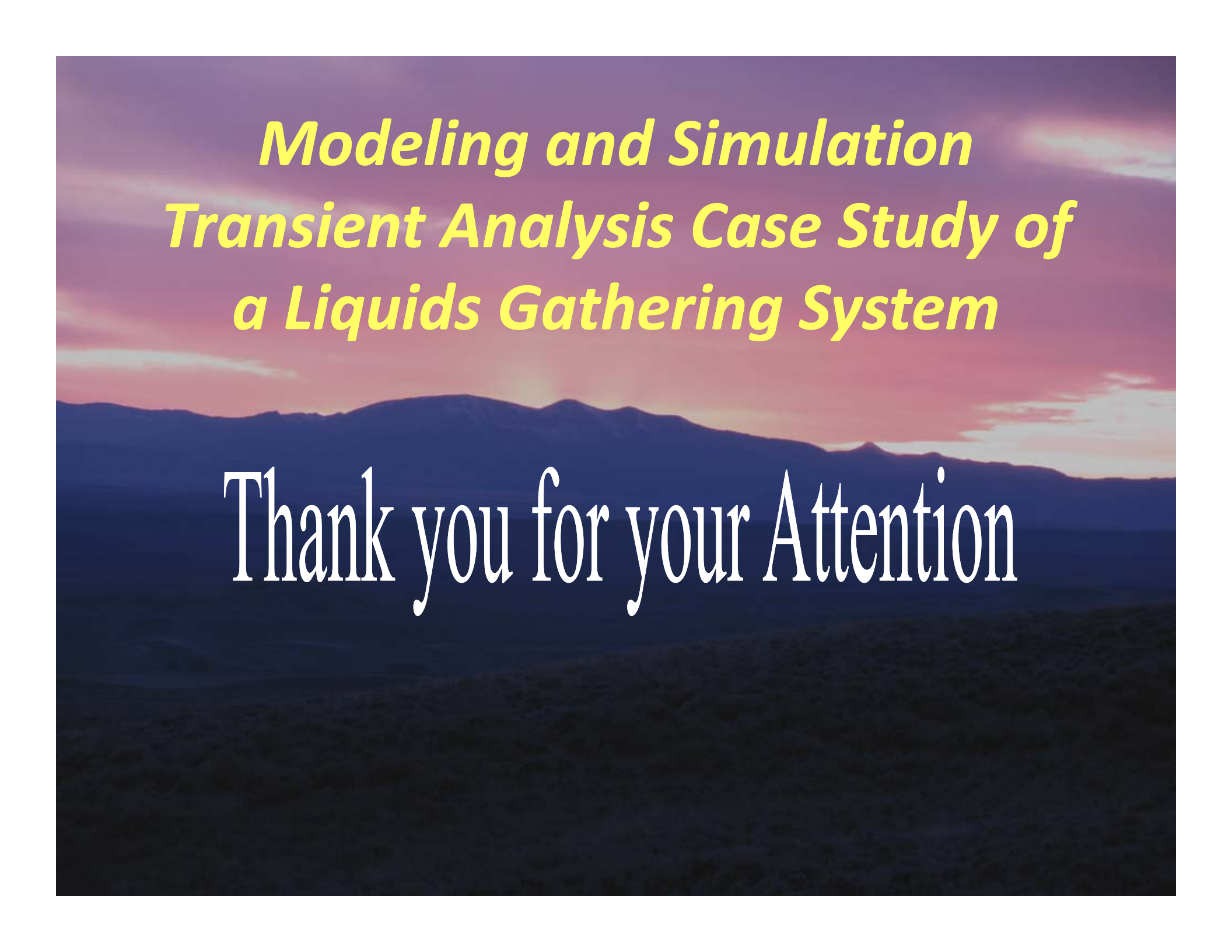
- ❖ We theorize the following:
 - Damage is incurred to the inner fibers due to the small pulsations, potentially from bending stress in the glass
 - This generates a weakness in the pipe which causes increasing stress in that area
 - Individual fibers continue to break further staining the remaining fibers
 - The failure of the outer fibers occur suddenly when the tensile strength of the fiber is exceeded leaving a clean break
 - As the glass layer is weakened the inner liner bulges outward before erupting through the outer liner

Failure Assessment, continued

- ❖ From an O&M standpoint, this would appear to be somewhat like operating a metal pipe above the endurance limit with pulsation
- ❖ Even a small pulsation can eventually lead to pipeline failure
- ❖ Once a failed area is repaired the stresses build up elsewhere

Summary & Conclusions

- ❖ Failures likely due to small cyclic stresses in the glass fibers
- ❖ Lesson learned, verify that your assumptions are correct and review all data in the field when provided the opportunity
- ❖ No evidence to support water hammer as an issue for either the 4-inch or 8-inch pipeline
- ❖ The revised operating philosophy is a substantial improvement over that of the pre-existing system
- ❖ Pulsations are not a significant threat to the integrity of the 8-inch steel pipeline, but may be a significant factor in the failure of the 4-inch pipeline



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Thank you for your Attention