

Getting Control for Optimal Plant Control



Improving Processes. Instilling Expertise.



Agenda

- Feeding the crusher
- Automation



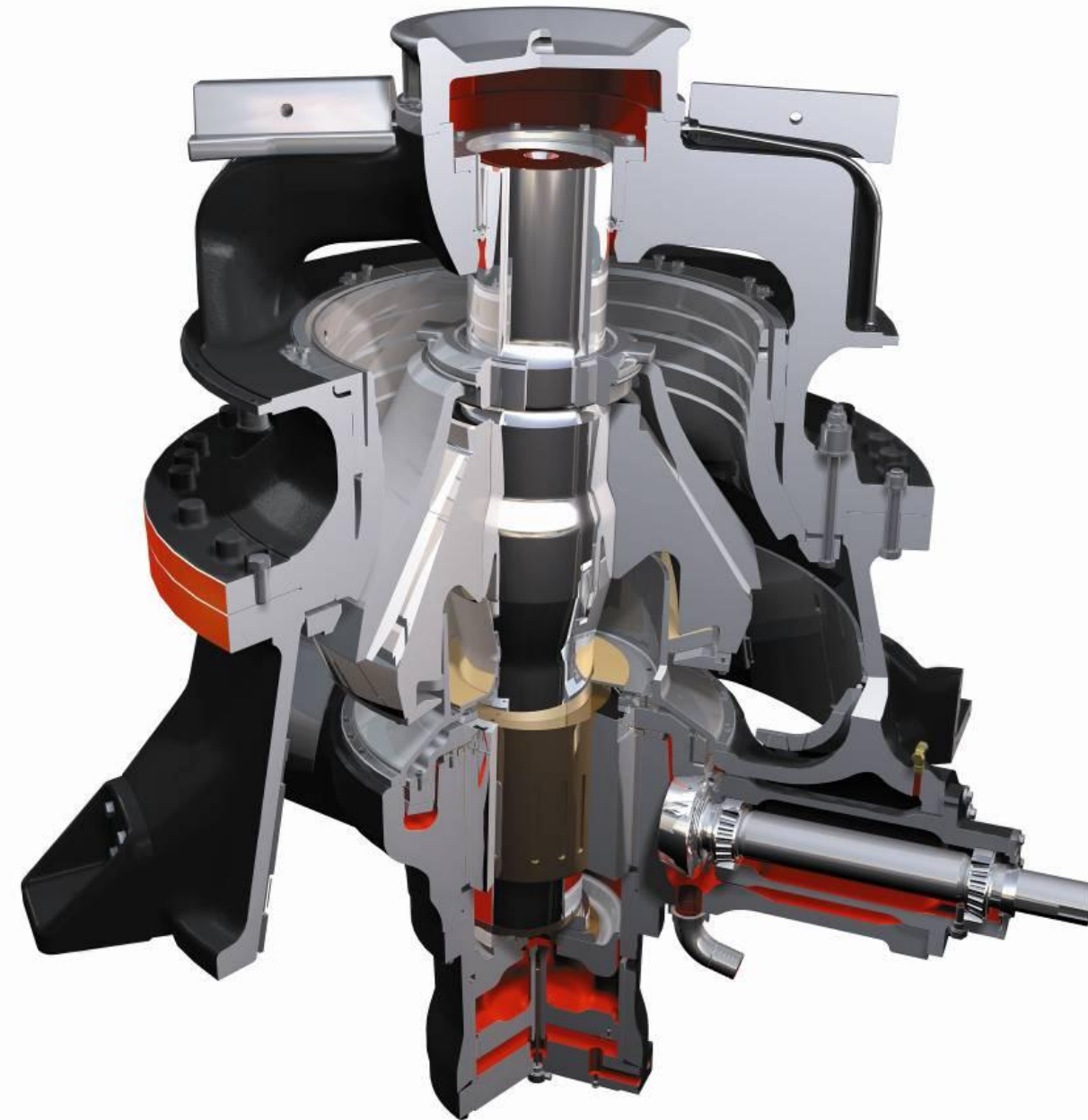
Feeding Arrangements

- The negative effects of poor feeding--- how poor feeds cause extra costs to the operation and reduce productivity
- Some ideas how we can determine the source.
- Some ideas how to prevent and cure, reduce costs, increase plant and equipment utilisation and generally increase profitability.

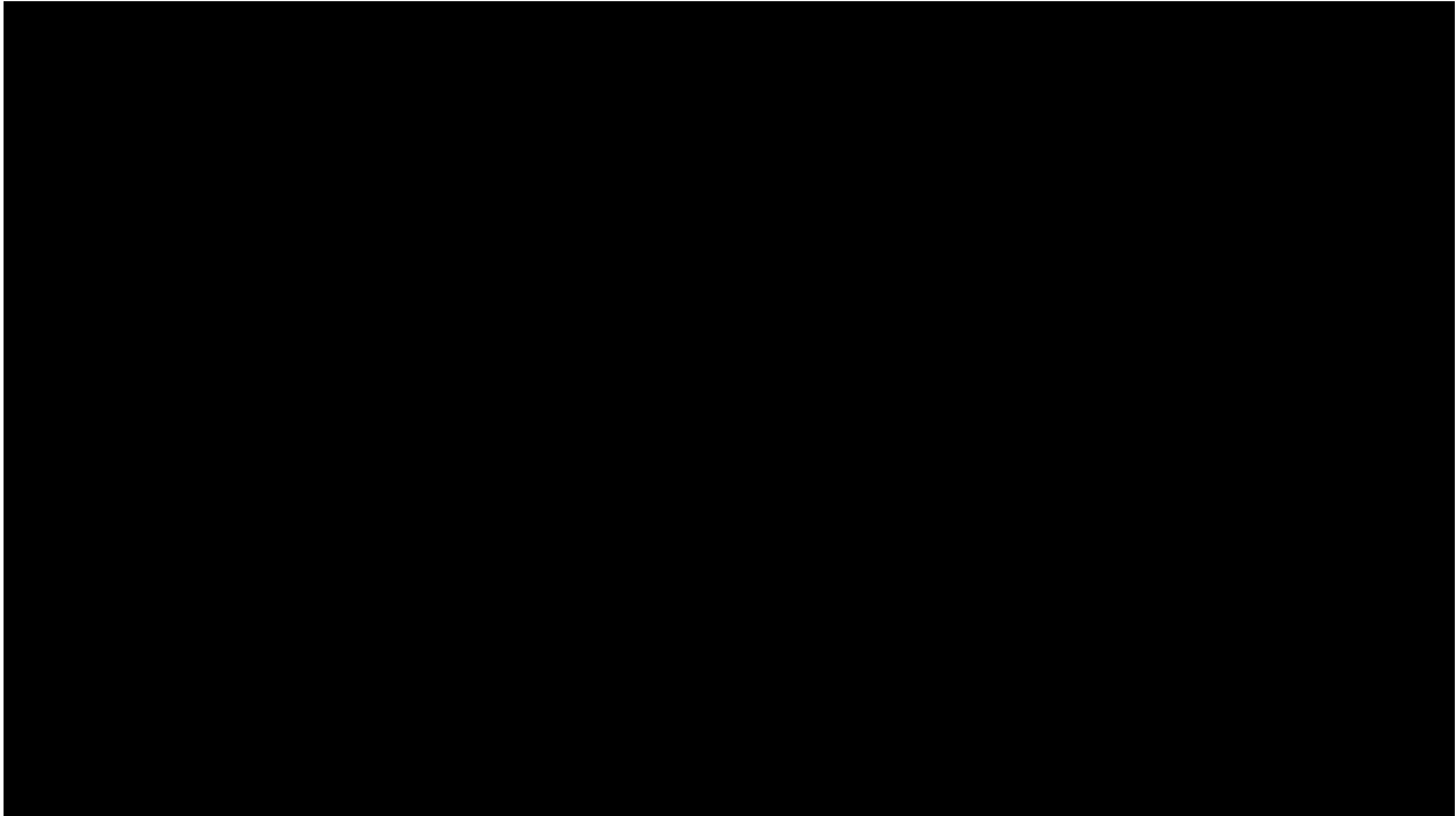


Cone Crusher Function

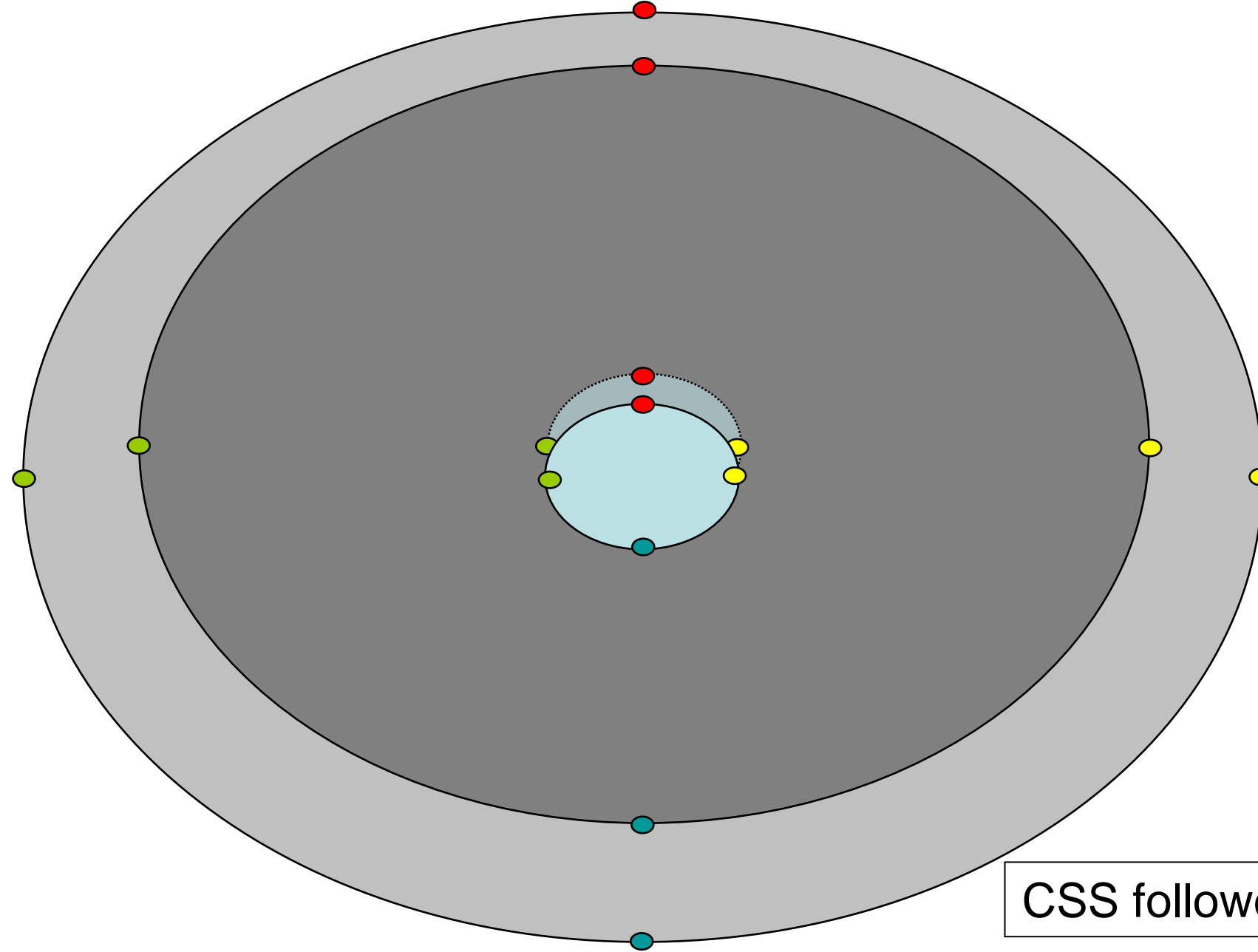
- The CSS runs around the chamber so the action is basically rotational.
- Raw material enters the chamber on the OSS and is crushed one half revolution later by the CSS.
- This cycle takes place in most cone crushers 5 to 6 times per second.
- Cone crushers have volumetric capacities.



Function sc.



Function

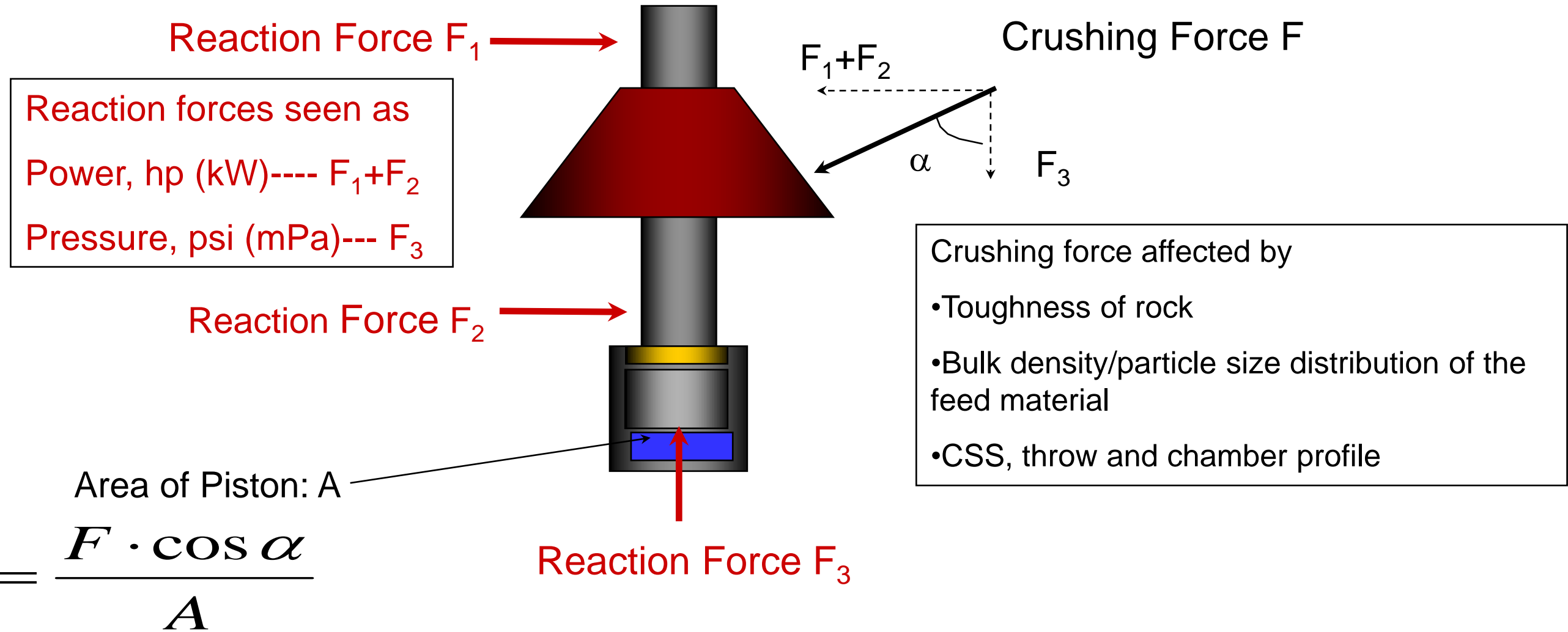


Concave

CSS followed 180° later by OSS

Reaction to well distributed, unsegregated feed

A similar crushing force will be seen throughout each and every revolution



$$p = \frac{F_3}{A} = \frac{F \cdot \cos \alpha}{A}$$

Segregation



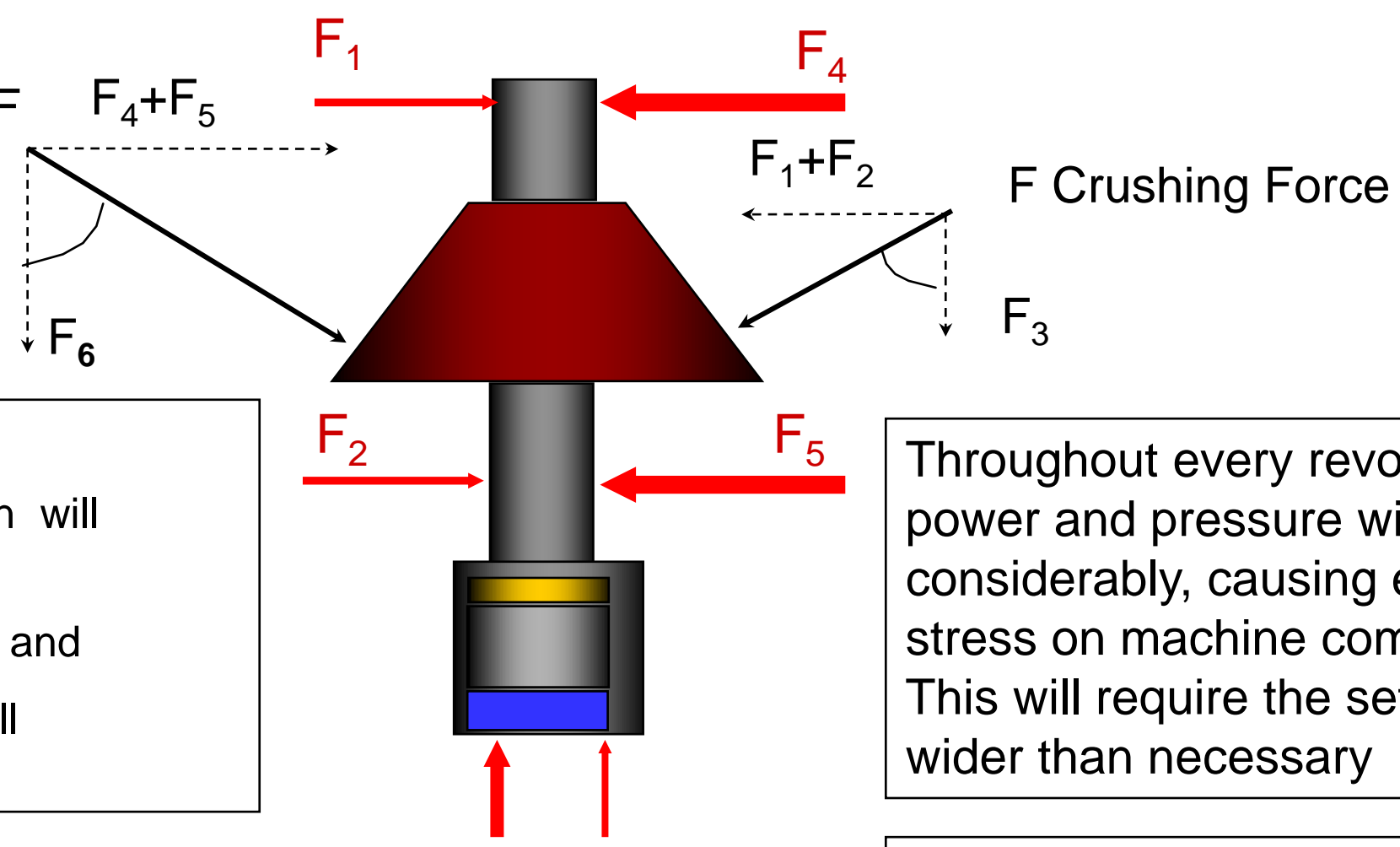
Possibly the greatest single factor in destroying crusher performance and process control.

Reaction to uneven, segregated feed

Crushing Force F

$$F_4 + F_5 > F_1 + F_2$$

$$F_6 > F_3$$



As wear becomes uneven

- the power and pressure fluctuation will become exaggerated,
- the setting more difficult to control and
- the product grading and quality will deteriorate.

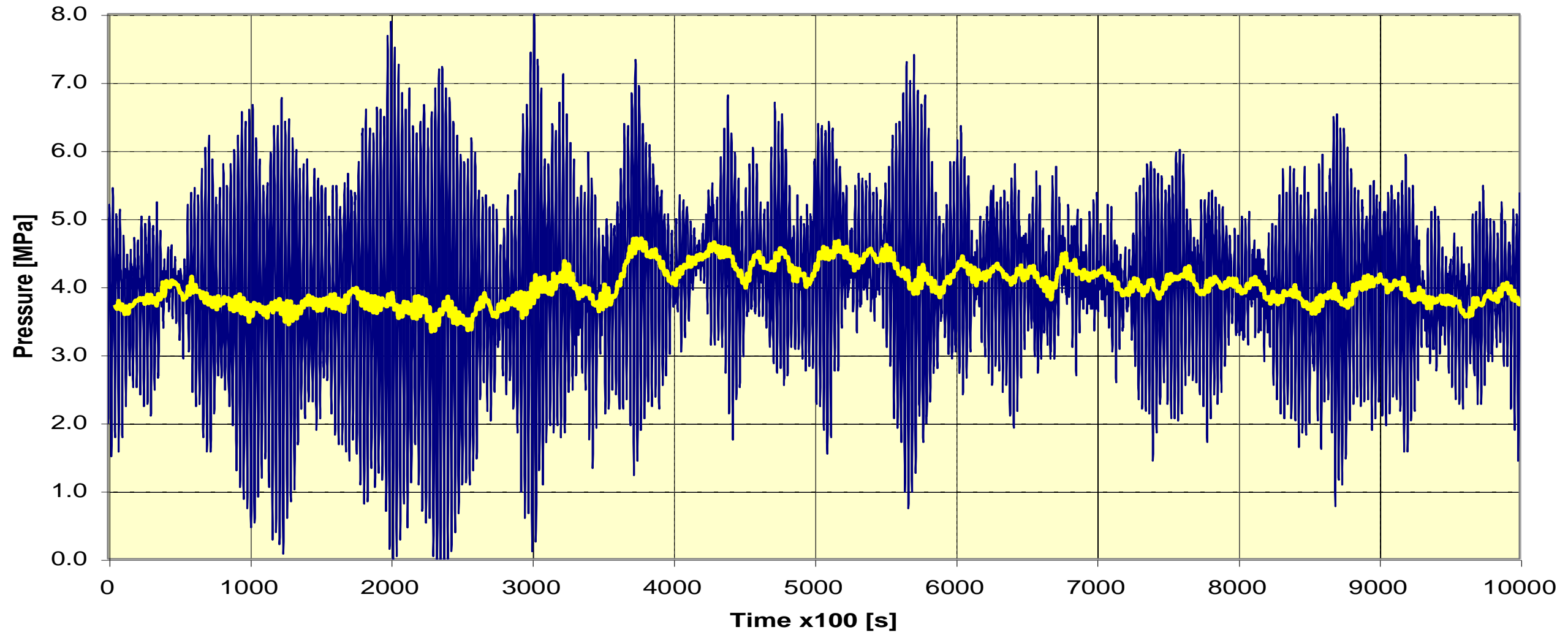
Throughout every revolution both power and pressure will fluctuate considerably, causing extreme cyclic stress on machine component parts. This will require the setting to be run wider than necessary

Zero reaction at any point during the revolution will suggest a portion of the chamber is empty

CH880, tertiary application

Misaligned/segregated feed - High pressure amplitudes

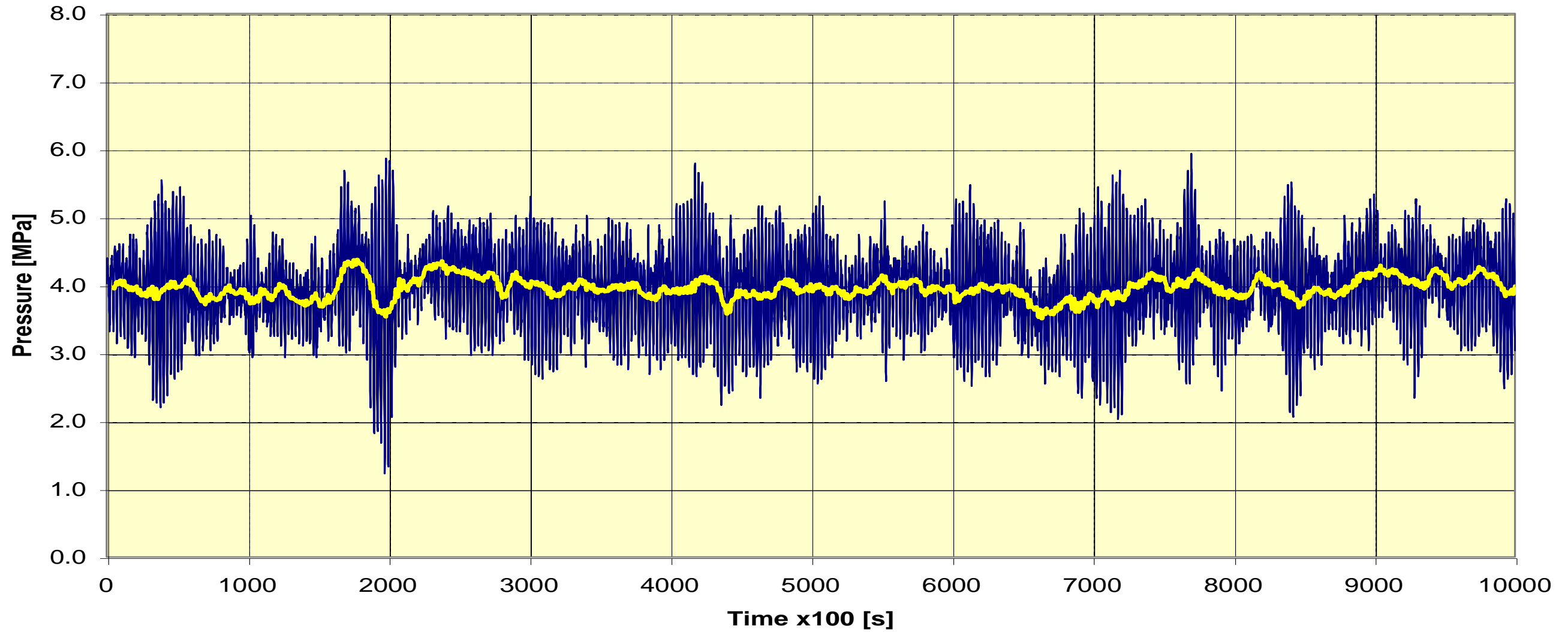
Misaligned Feed



4mpa=580psi

Improved segregation

Aligned feed- Low pressure amplitudes
Aligned feed



4mpa=580psi

What are the negative effects?

High power and pressure will cause the crusher to be run at wider than necessary settings resulting in coarser product therefore higher recirculating loads with increased conveying, wear and crushing **Costs**.

Higher circulating loads leads to lower system feed, **less product on the ground**.

Occasionally the necessity for increased crushing will demand **increased capital investment**.

Segregated and poorly distributed feeds will cause the crusher liners to wear unevenly, again with deteriorating performance and associated **Costs**.

Product will become coarser and less cubical. **Costs??**

What are the negative effects?

Segregation and uneven wear will cause reduction in liner life through premature exchange. **Costs??**

Segregation and uneven wear will cause reduction in mechanical component life, often leading to traumatic failure and the **costs of unplanned stoppages.**

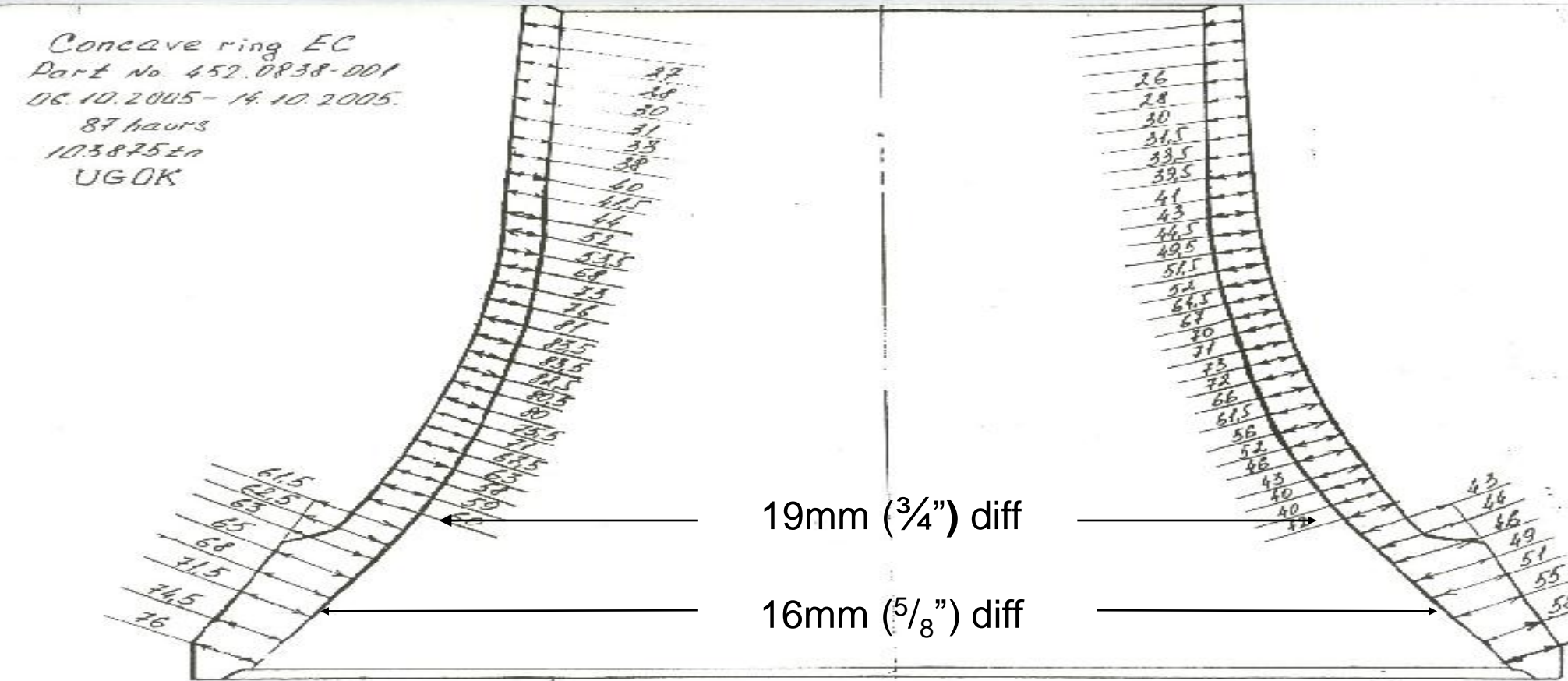
ALL IN ALL CONSIDERABLE COST TO THE OPERATION.

Case study Segregation

CH870 EC Iron ore

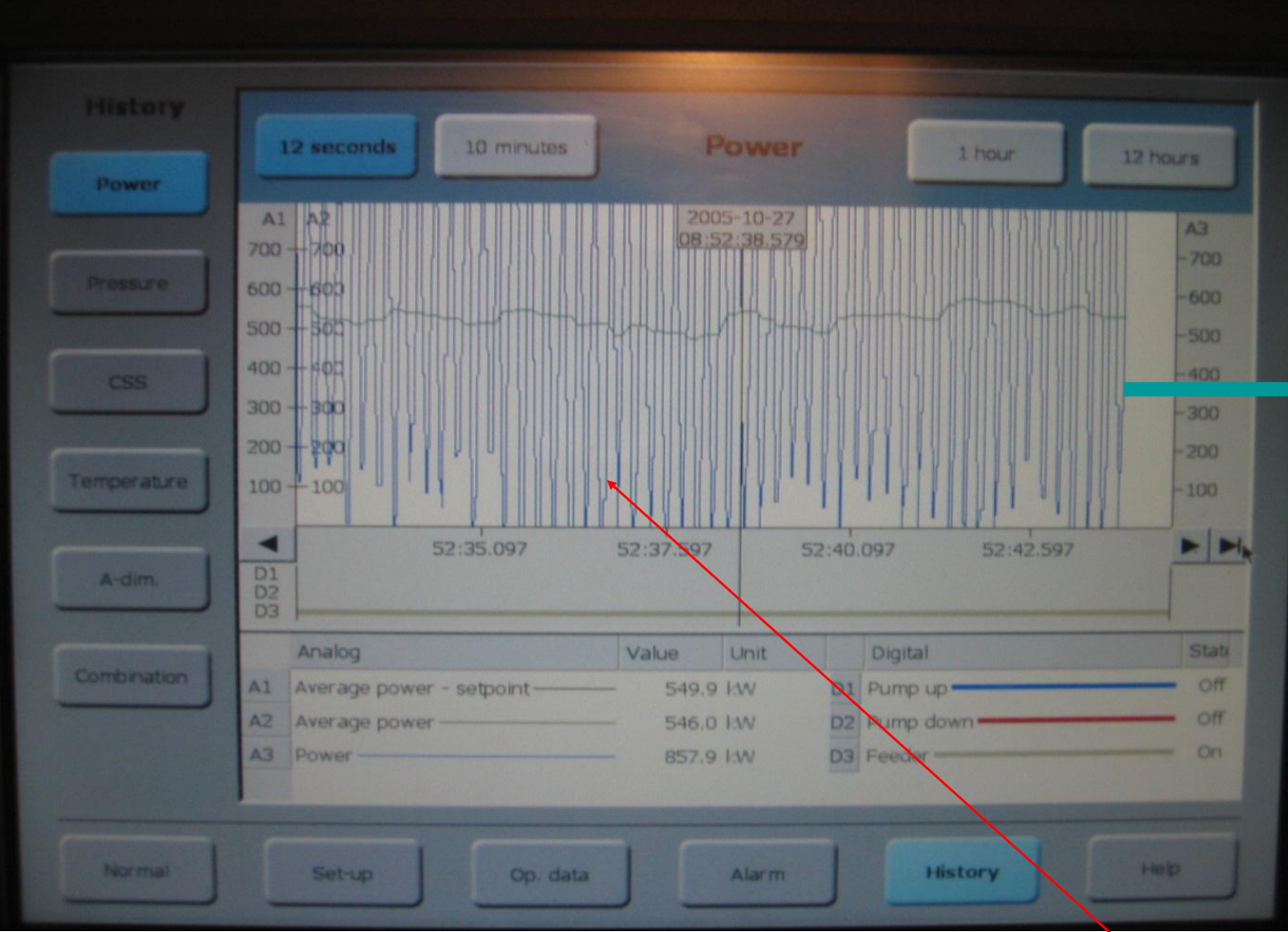


Negative effect of uneven wear



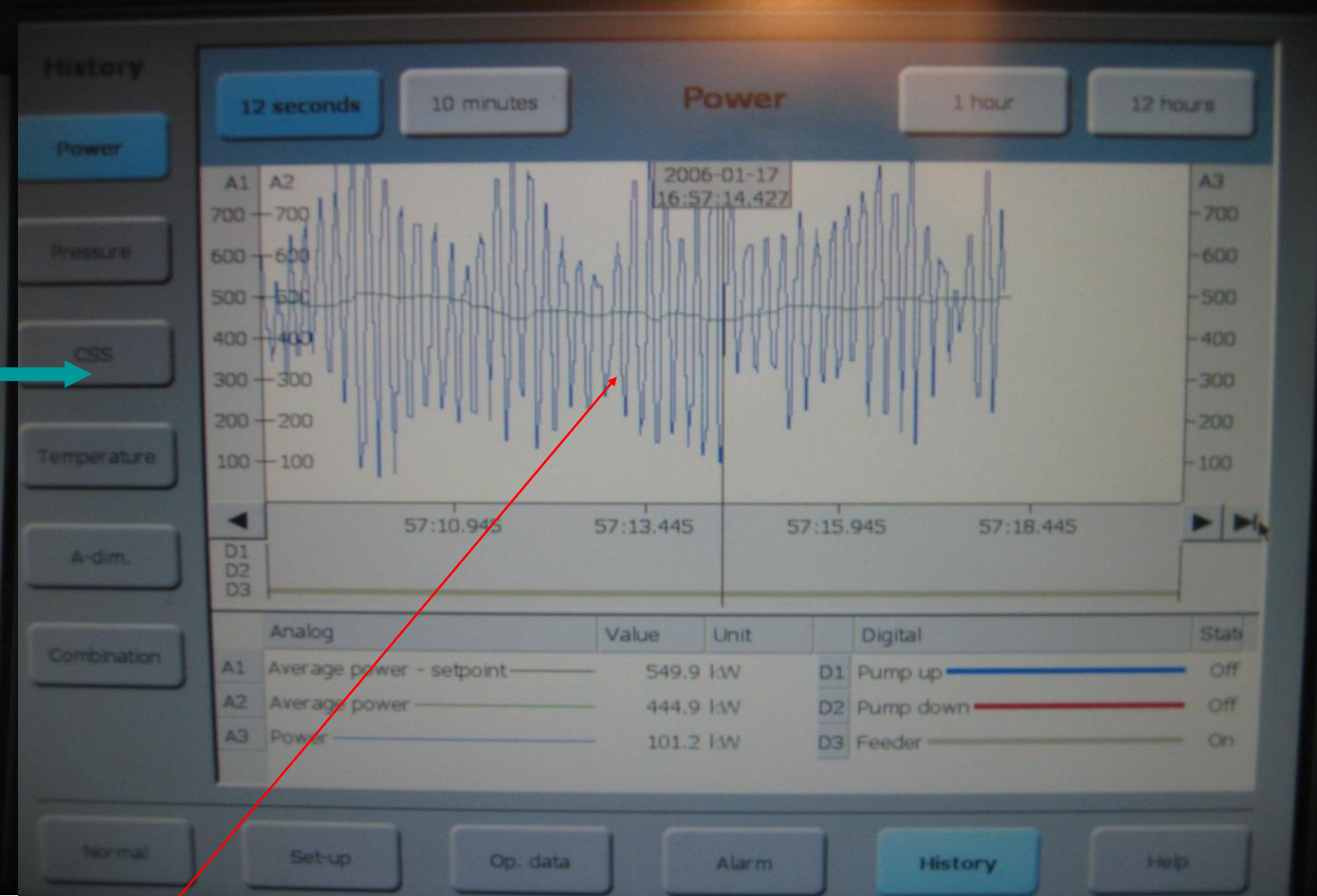
Demands much higher scrap weight----increased operating costs

Improvements after fitting an RFD



27. 10. 05

Each amplitude represents 1 cycle



17. 01. 06

500kW=670hp

History

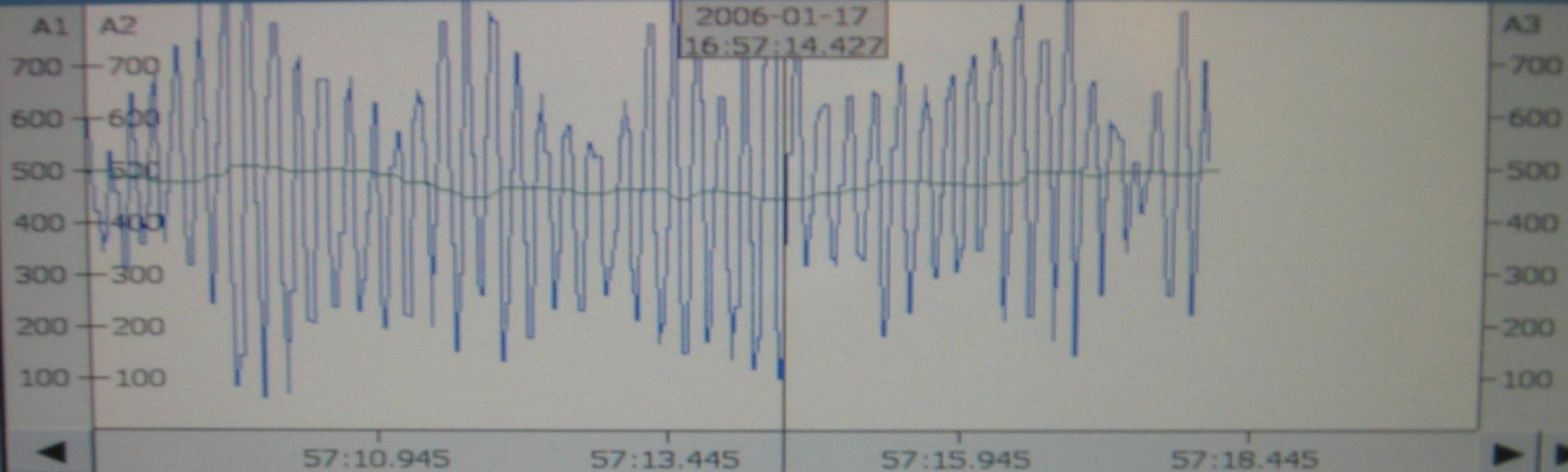
12 seconds

10 minutes

Power

1 hour

12 hours



57:10.945 57:13.445 57:15.945 57:18.445

	Analog	Value	Unit	Digital	State
A1	Average power - setpoint	549.9	kW	D1 Pump up	Off
A2	Average power	444.9	kW	D2 Pump down	Off
A3	Power	101.2	kW	D3 Feeder	On

Normal

Set-up

Op. data

Alarm

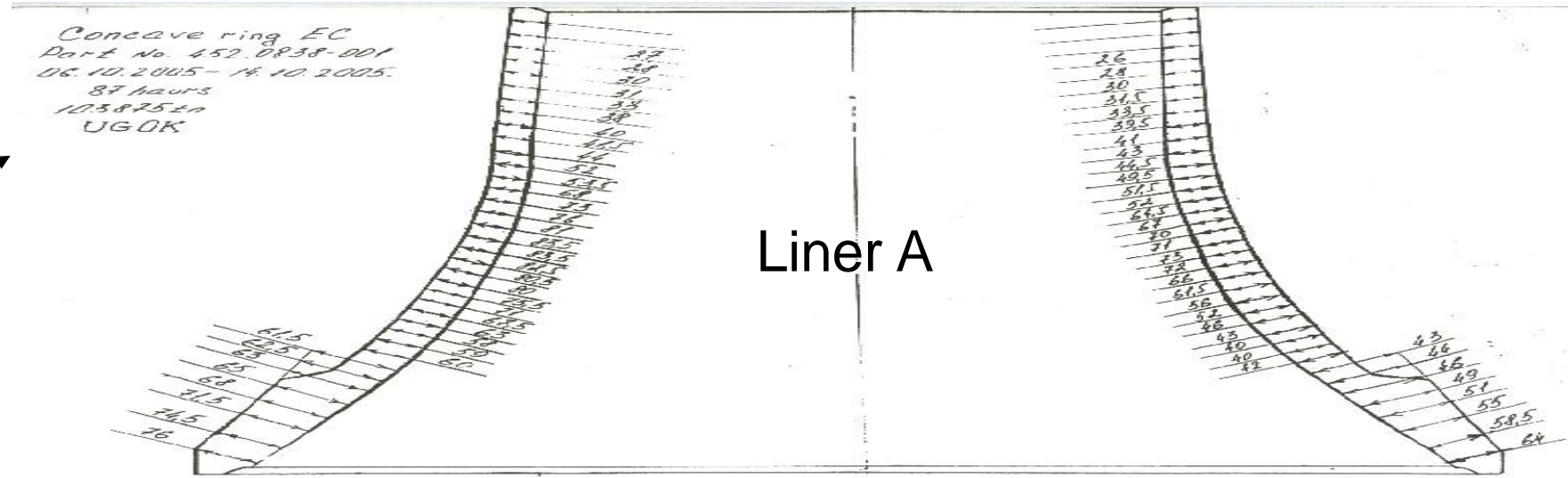
History

Help

500kW=670hp

Wear life improvement after fitting RFD

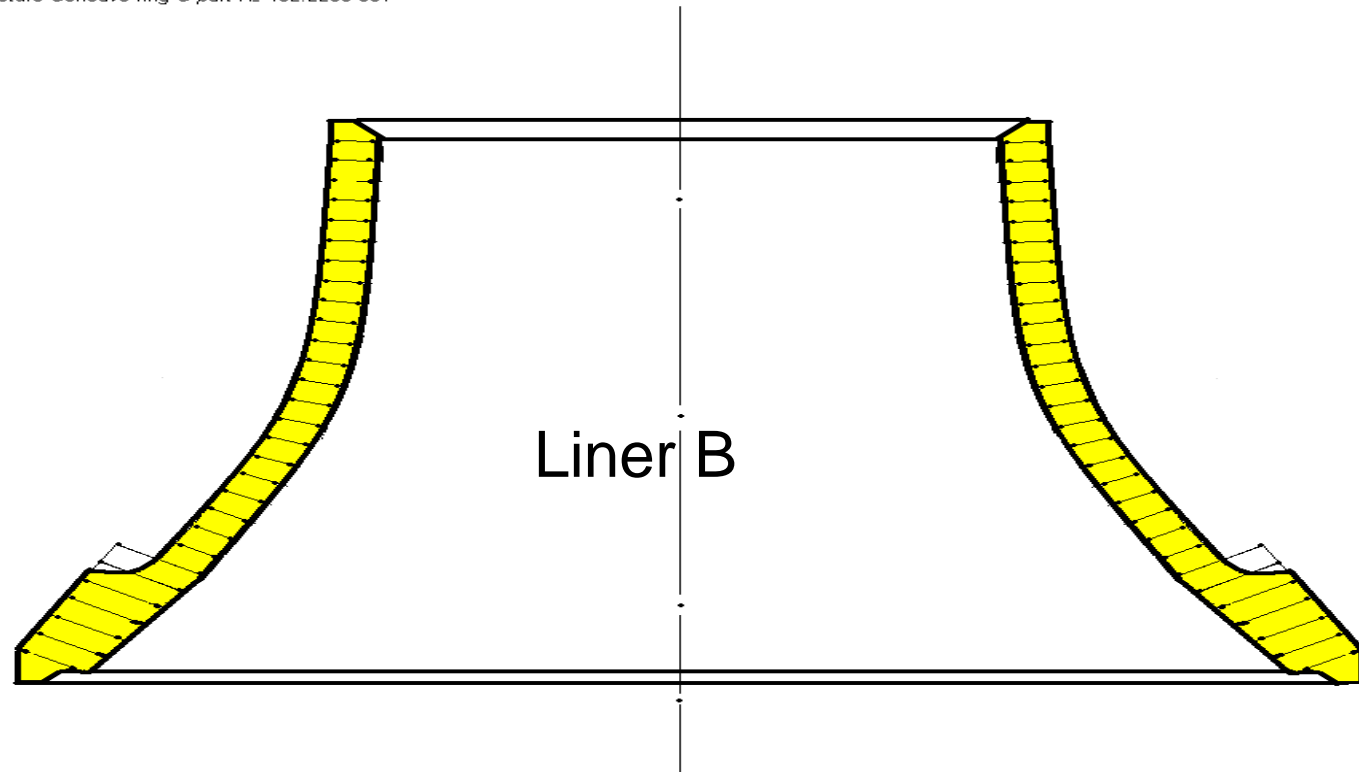
87 hours
 103875 tonnes (114470stons)
 1194 mtph (1316stph)



166hours
 145311 tonnes (160133stons)
 875 mtph (965stph)

This information will tell o structure Concave ring C part No 452.2255-001
 Operating time of 166 hours
 Ore processing 145311 tons
 The size A before 297 mm
 The size A after 131 mm

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Cost comparison

	Liner A	Liner B
Hours	87	166
Tons	114470	160133
Tons/hr	1316	965
Average setting over liner lifetime	3 ³ / ₁₆ " (80mm)	2 ³ / ₈ " (60mm)
Differential wear	3/4" (19mm)	3/16" (5mm)
% oversize	47	22
Tons/hr oversize	619	212
Tons/hr product	697	753
Additional cost assuming \$0.5/ton	\$310/hour	\$106/hour
Wear cost (assuming \$10000 per set)	10000/(697 x 87) =\$0.165/ton of product	10000/(753 x 166) =\$0.08/ton of product

Costings are for comparative purposes only

Early Prevention

- During the design stage, whether a new plant or plant extension or replacement crusher is being planned, careful consideration is required to the design of the feeding arrangement.
- Material normally arrives in a stream, from a conveyor, feeder or chute—the need is for even full width distribution with no segregation.
- Height can be an ally when available and employed to constrain material, change flow direction, combat segregation and remove impact, but a deadly enemy when working against us--too little height gives no opportunity.

Early Prevention

- **Flexibility in design---e.g.... the opportunity to alter the position and speed of the material discharge point and trajectory.**
- **Each feed arrangement design is unique, can be complex and may require several compromises**
- **THE OPERATIONAL SUCCESS AND OVERALL OPERATING COST OF THE INSTALLATION WILL DEPEND ON A SATISFACTORY DESIGN.**

Late cure

WHY segregation?

- In general conveyor belts.
- Narrow high speed belts.
- Elevated material fed with a trajectory.
- Transfer points discharging at angles
- Conveyors to bins

Belt width and speed



Belt width and speed



Static distributors and splitters













Summary

Poorly designed crusher feeds leading to segregation or uneven distribution are extremely costly and often remain so for the life of the operation. These costs result from:

- 1. Re-crushing oversize through running crushers wider than necessary.**
- 2. Detrimental effects on product quality.**
- 3. In serious cases increased capital expenditure**
- 4. Energy and wear costs as oversize is transported around the plant.**

Summary

- 5. Poor utilisation of manganese liners through uneven wear.**
- 6. Poor utilisation of component parts through extreme cyclic overloading.**
- 7. In serious case traumatic unplanned mechanical failures.**
- 8. Lost business opportunities.**

Improved feeding

I hope we have given an insight into some causes, consequences and possible solutions to poor feeding.

Segregation and /or poor distribution, if they already exist can and should be improved.

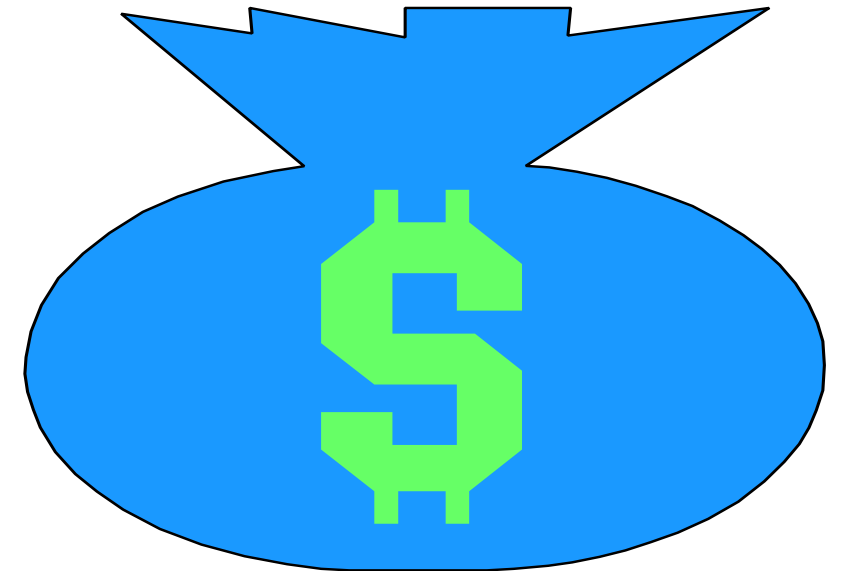
Automation - Control

Audience Survey

- How many of you have some form of automation in your plants today?
- How many of you have some form of automation on your cone crushers today?

Why Automation Control ?

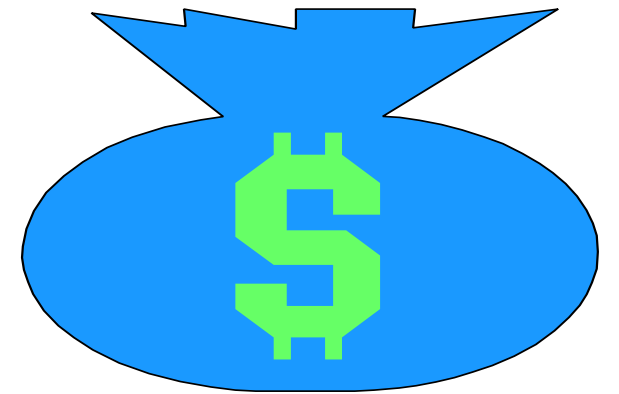
- Repetitive conditions
- Free up man power
- Increase reaction time
- Control a system remotely
- Increase efficiency of a system
- Maximize efficiency of a piece of equipment
- Increase product quality
- Protect capital investment
- Optimize a particular product
- Monitoring operation
- Data gathering





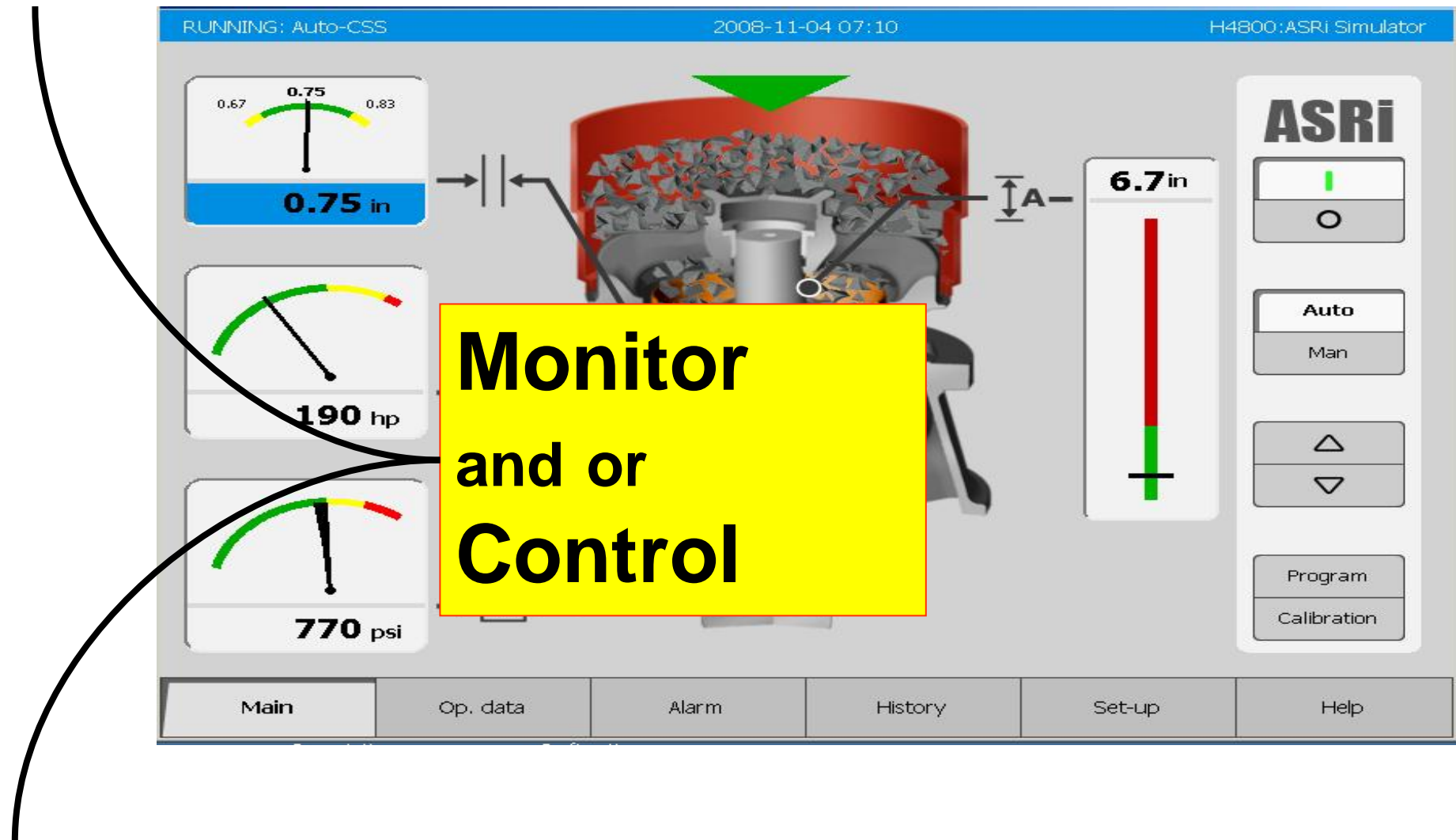
WHY AUTOMATE YOUR CONE CRUSHER ?

- Realize a higher return on your investment.
 - Higher net production of desired products
 - Optimum power utilization
 - Continuous generation of quality products
- Protection of your investment
 - Constant overload protection
 - Continuous adjustment compensating for changes in material characteristics
 - Ability to analyze operational data



Monitor and Control Available at a push of a button

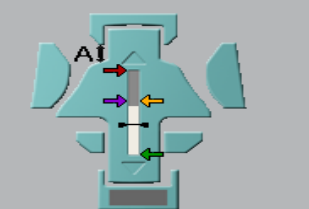
- Closed Side Setting
- Horsepower in use
- Power consumption
- Load Time
- Operating time
- Hydraulic Pressure
- Lubrication Oil temperature
- Liner Wear
- Recorded data
- Graphing data



ASRI

Select program | Edit program | Calibration

Description



A-Min	15.0 mm
A-Cal-Calculated	41.3 mm
A-Cal-Latest	41.3 mm
A-Bottom	100.5 mm
Current	65.2 mm

A-Min A-Cal-Calculated
 A-Cal-Latest A-Bottom
 Current

Mantle Position Calibration & Liner Wear

Auto
P1, Auto-CSS
Setpoint: 12.0 mm




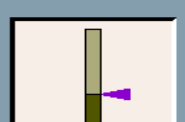
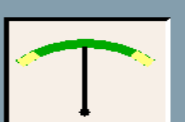
M - M Lead

Close Stop

Normal Set-up Op. data Alarm History Help

Op. data

Combination

Power	Pressure	Lub. oil temp.	A-dimension	CSS
				
98 kW	3.4 MPa	0.0 C	69.7 mm	14.9 mm

Operating time (h)	Total	Loaded	
	Since original start-up	15	5
	Since latest liner change	8	2
	Since latest calibration	8	2
Since resetting	0	0	

Energy consumption (MWh)

Since original start-up	0.4
Since resetting	0.0

Combined Status Listing

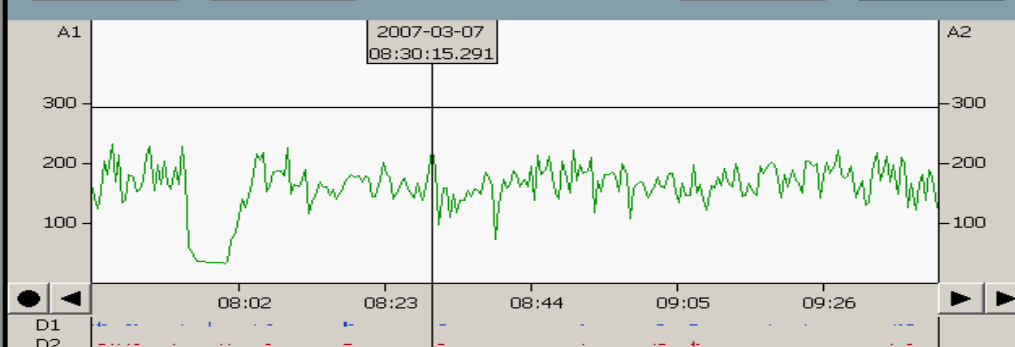
Normal Set-up Op. data Alarm History Help

ASRI Reporter

History

Power

12 seconds 10 minutes 1 hour 12 hours



Analog	Value	Unit	Digital	Status
A1 Average power - setpoint	294.8	hp		Off
A2 Average power	190.3	hp		Off
			D2 Pump down	Off
			D3 Feed r...	On


Historical Activity Log

Normal Set-up Op. data Alarm History Help

Op. data

Temperature Return oil (C)

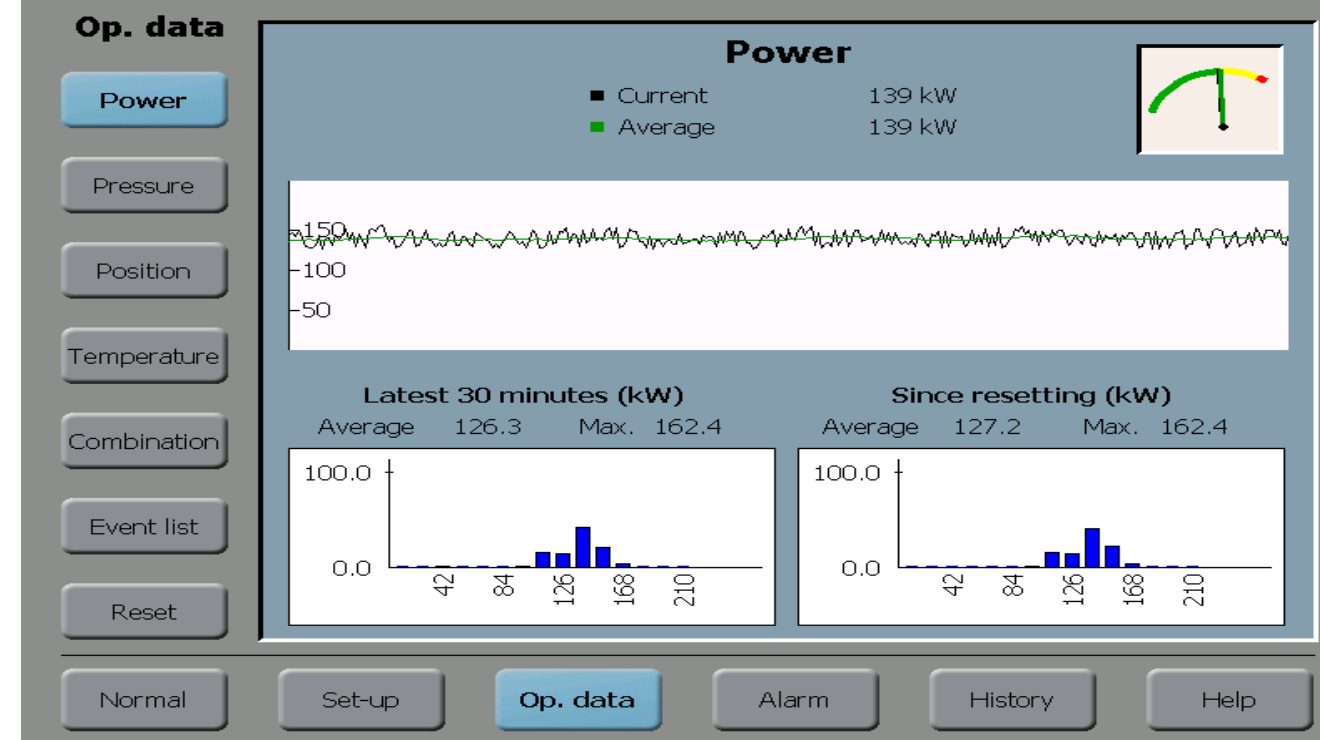
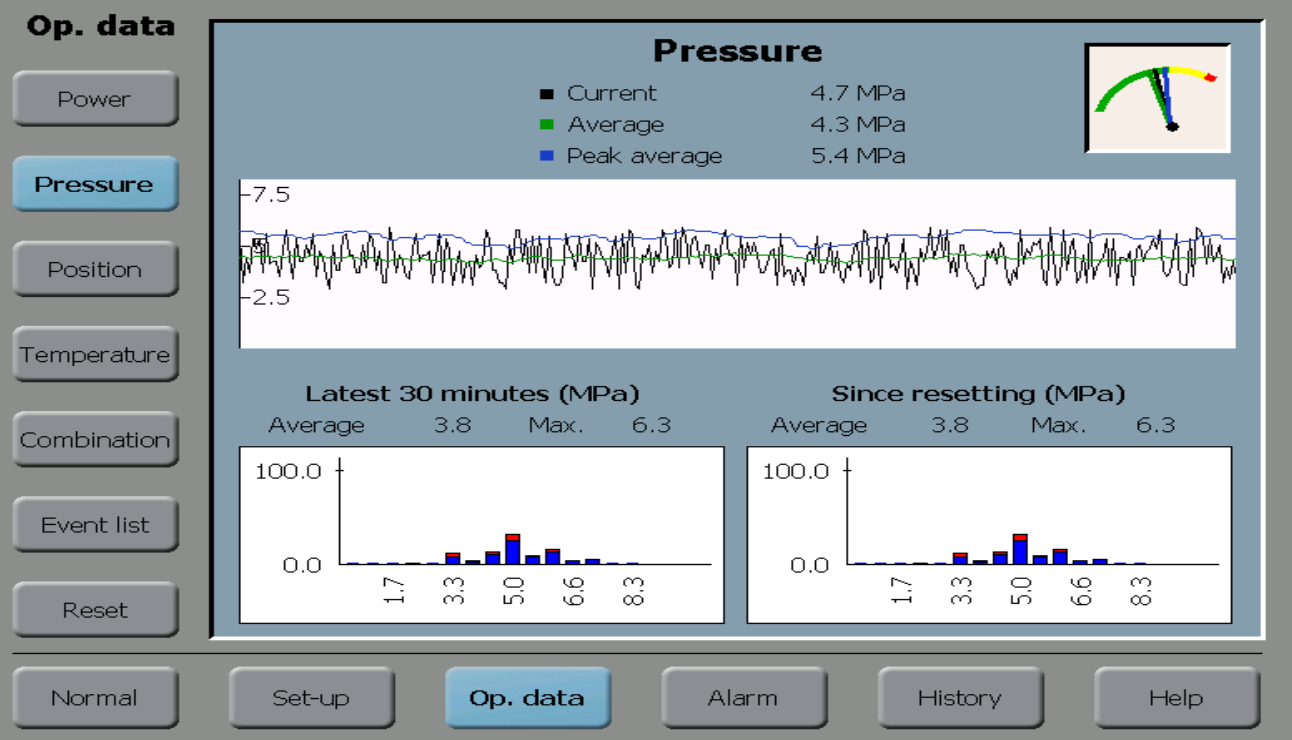
Current 0 C



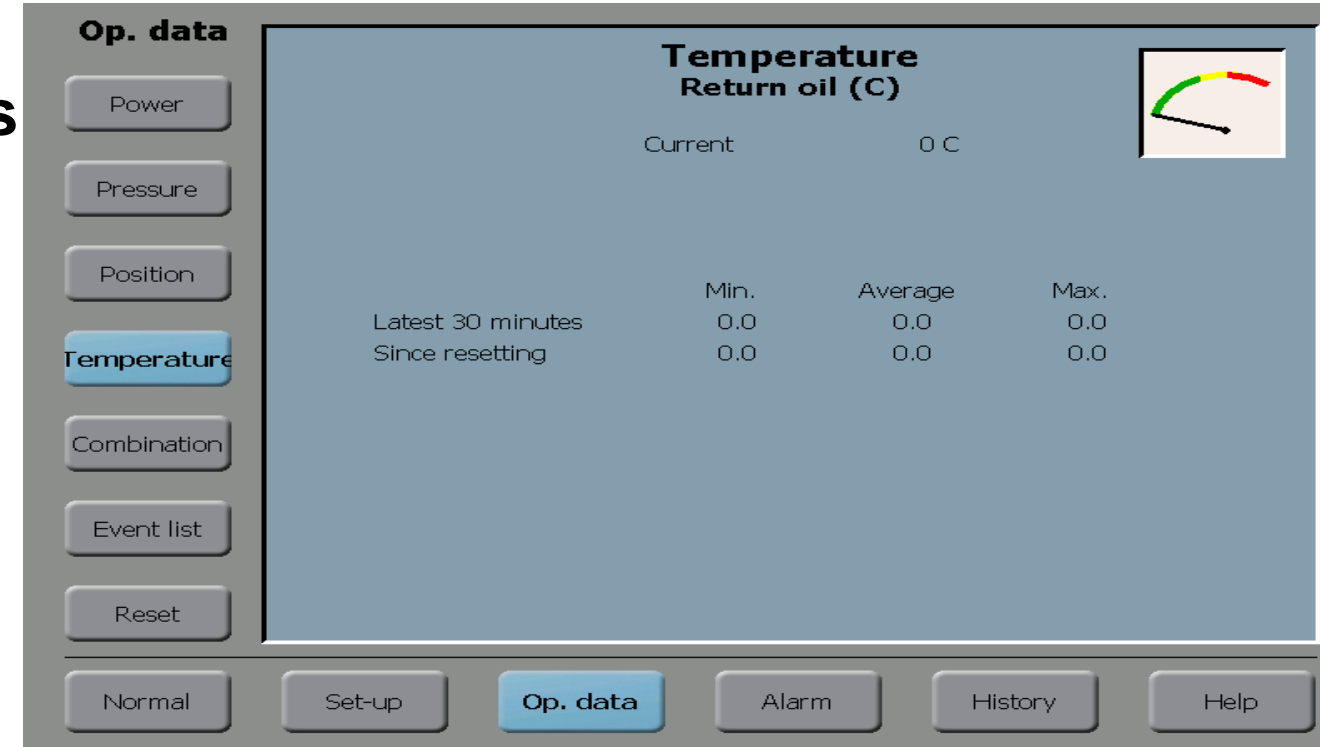
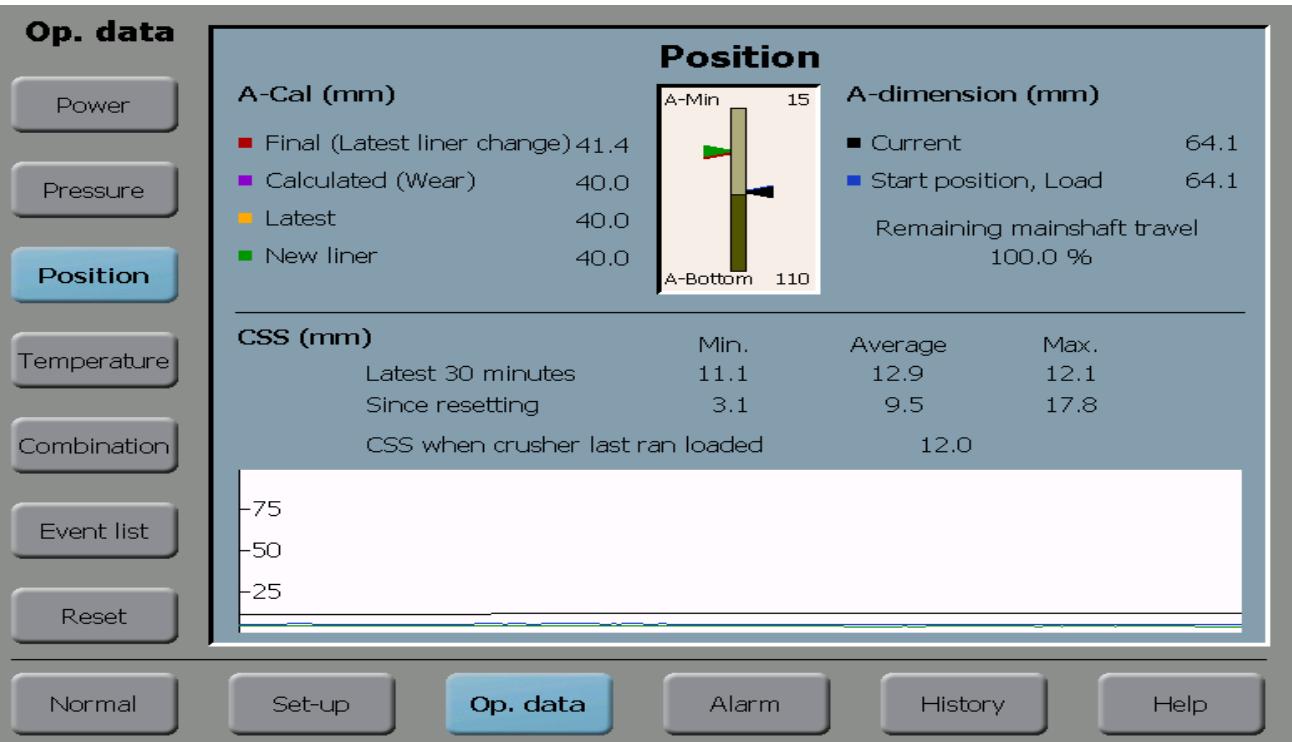
	Min.	Average	Max.
Latest 30 minutes	0.0	0.0	0.0
Since resetting	0.0	0.0	0.0

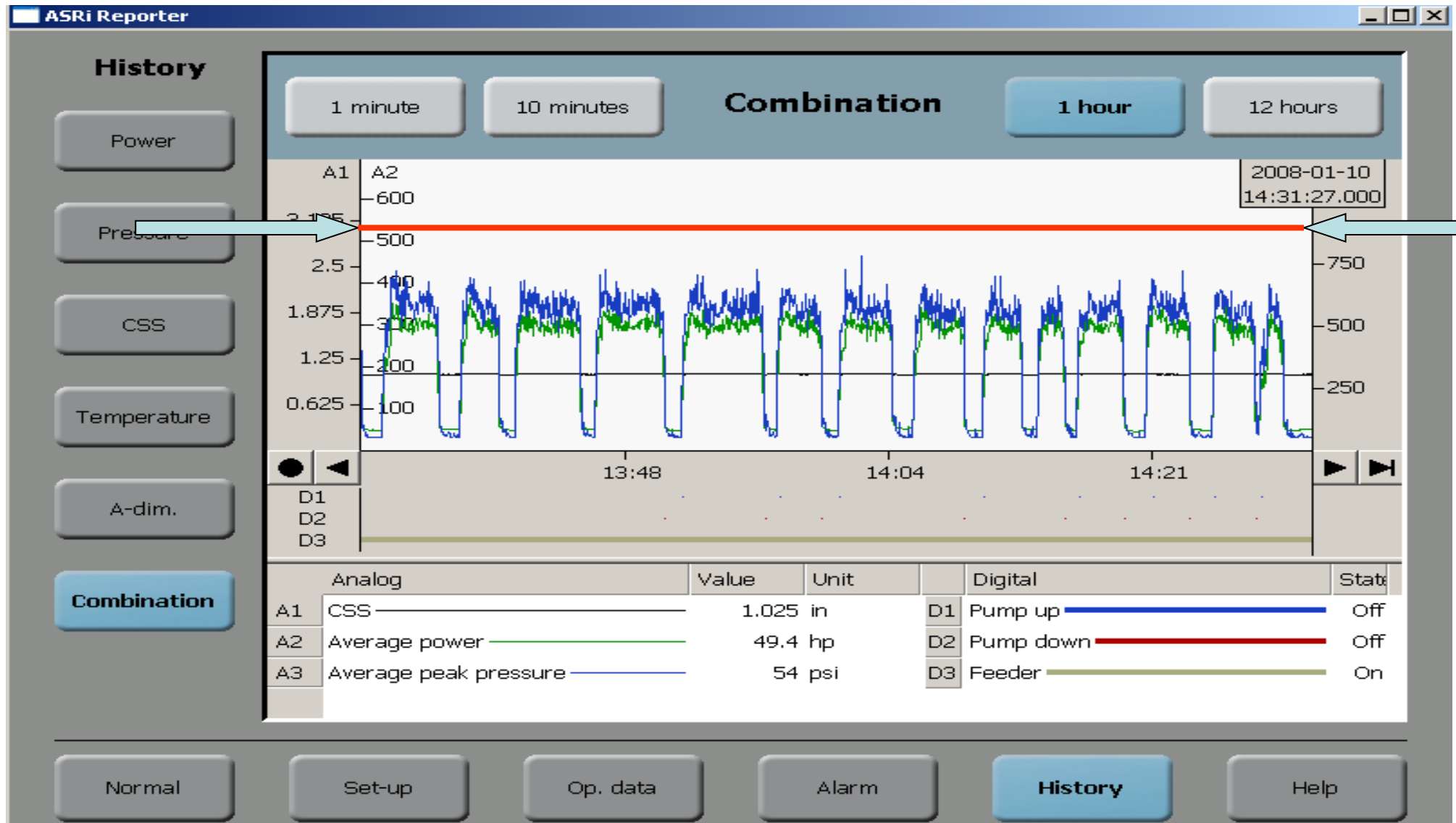
Lubrication Oil Temperature

Normal Set-up Op. data Alarm History Help

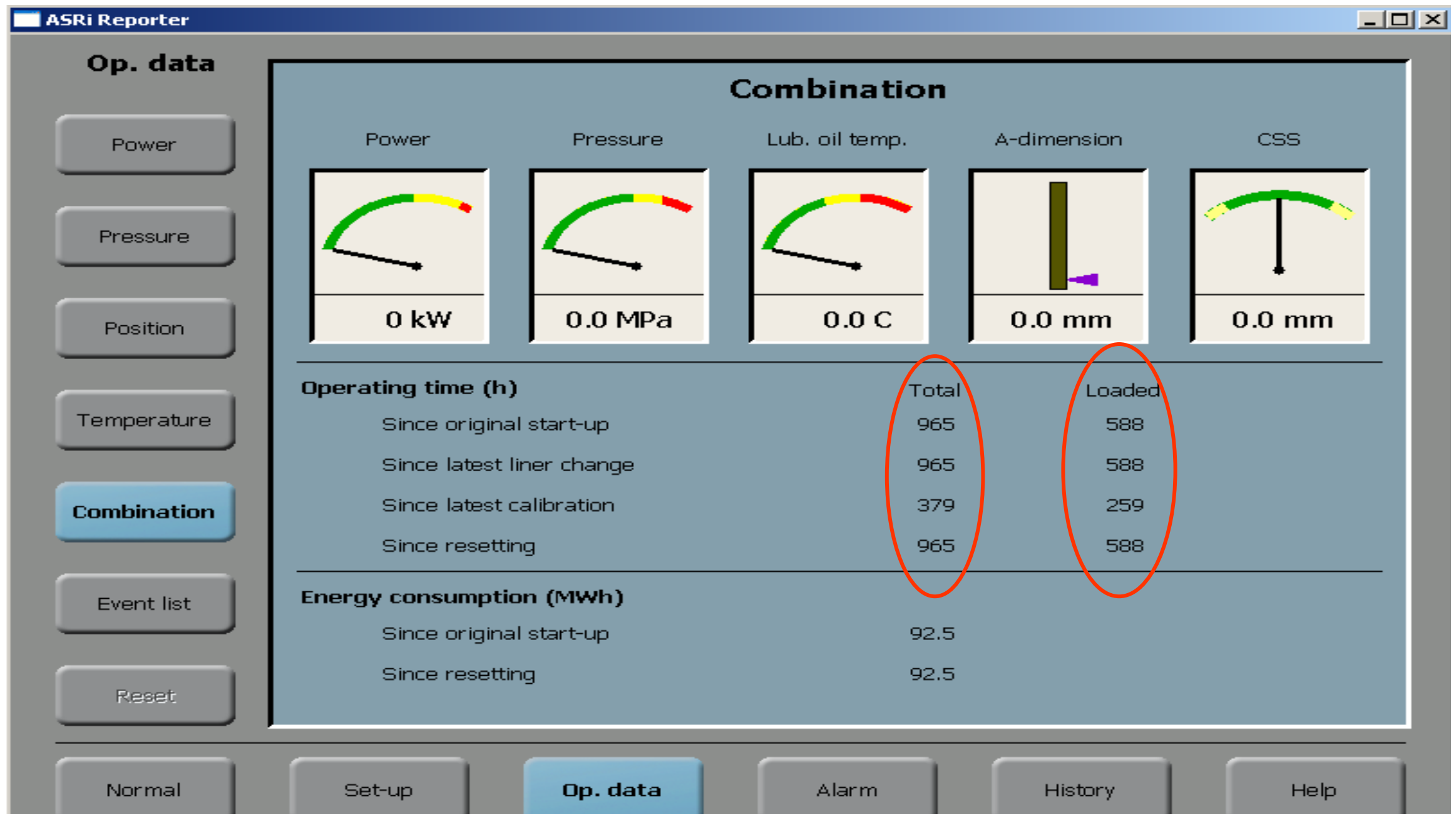


Historical Activity Logs





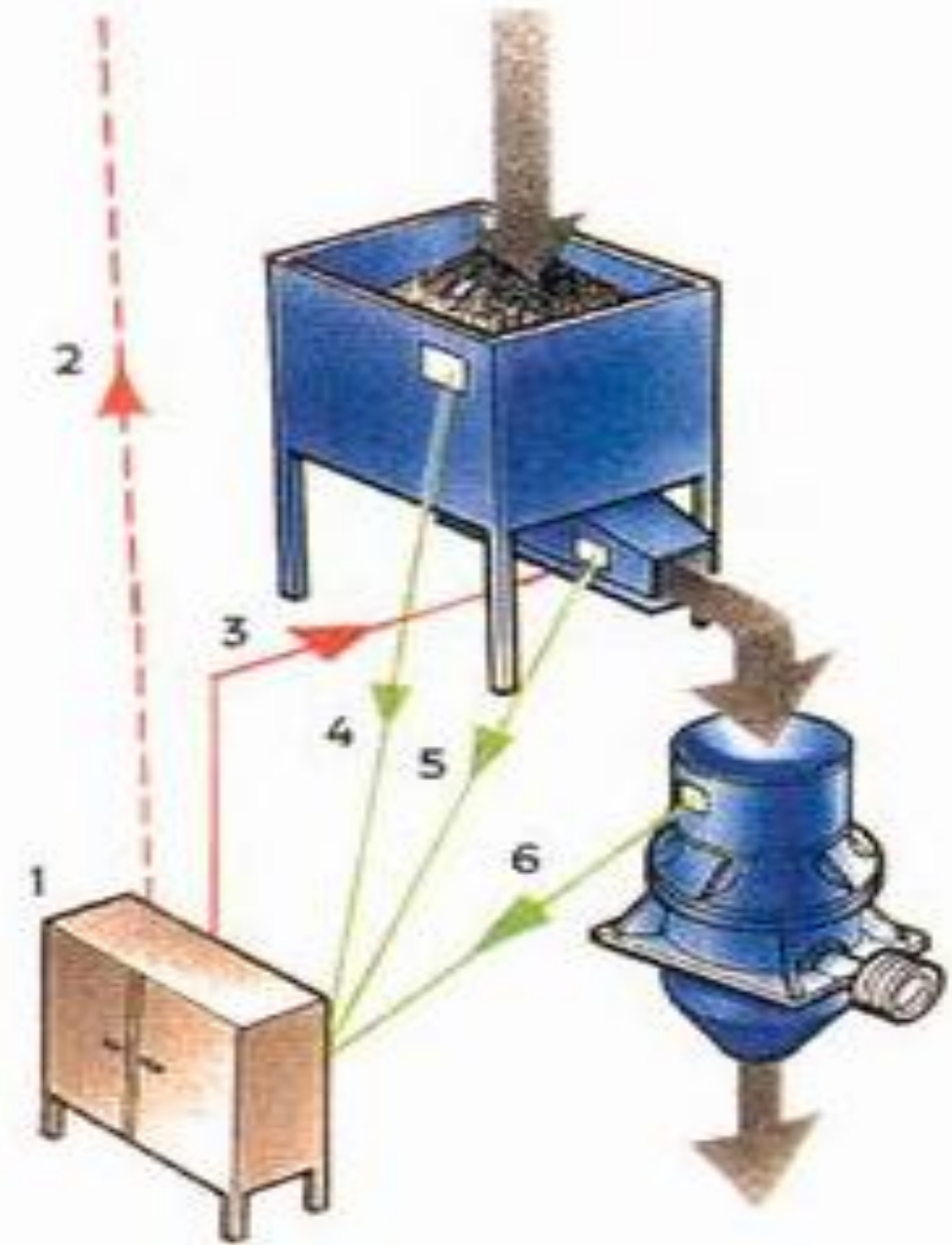
One Hour time span



Loaded 66% of an hour

System Automation & Control

1. Switch gear unit
2. Stop signal to feeder
3. Control signal to feeder
4. Max. level in surge bin
5. Min. level in surge bin
6. Max. level in crusher feed hopper



Automation

- Other things to consider
 - Automation mode vs Manual mode
 - Durability of use
 - Is the tool easily used

In summary automation of a compression crusher will provide:

- Higher net production of desired products
- Optimum utilization of motor power
- Continuous adjustment of setting to compensate for feed conditions.
- Full utilization of the units capacity
- Constant overload protection
- The ability to analyze operating data
- The opportunity to monitor the unit from remote location.

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Thanks for your attention



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